



Simulation of transients of DONES lithium loop with MELCOR fusion 1.8.6

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G. D’Ovidio, F. Martín-Fuertes
gianluca.dovidio@ciemat.es



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Introduction

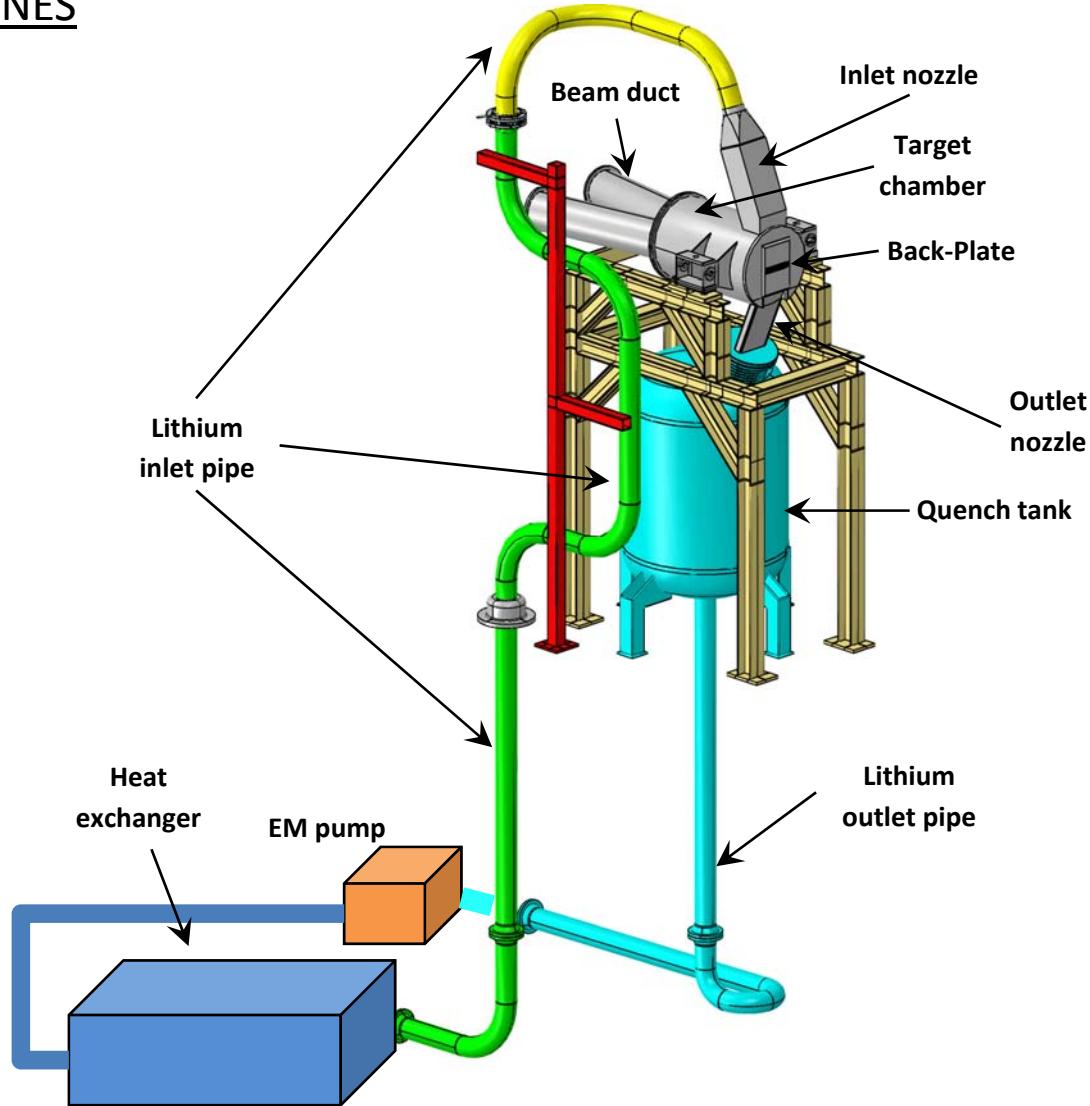


- ❑ According to the 2014 European Fusion Roadmap, an early construction of DEMO is expected by 2030
- ❑ A **DEMO-Oriented Neutron Source (DONES)** has been proposed to create a fusion material database required in a fusion reactor (based on “IFMIF” concept)
- ❑ The objective of the **Early Neutron Source (ENS)** project (EUROfusion/ WPENS) is to carry out activities for the engineering design development of DONES
- ❑ A safety analysis is required for DONES licensing and construction

- ❑ DONES deterministic safety analysis performed on selected reference scenarios (identified by FMEAs)
- ❑ Preliminary assessment of consequences to public and workers in support of DONES licensing
- ❑ In this presentation:
 - Operational transient sequence and **LOFA scenario** (with/without beam shutdown) of **DONES lithium loop**

DONES main Li Loop

3D Sketch of DONES
main Li Loop

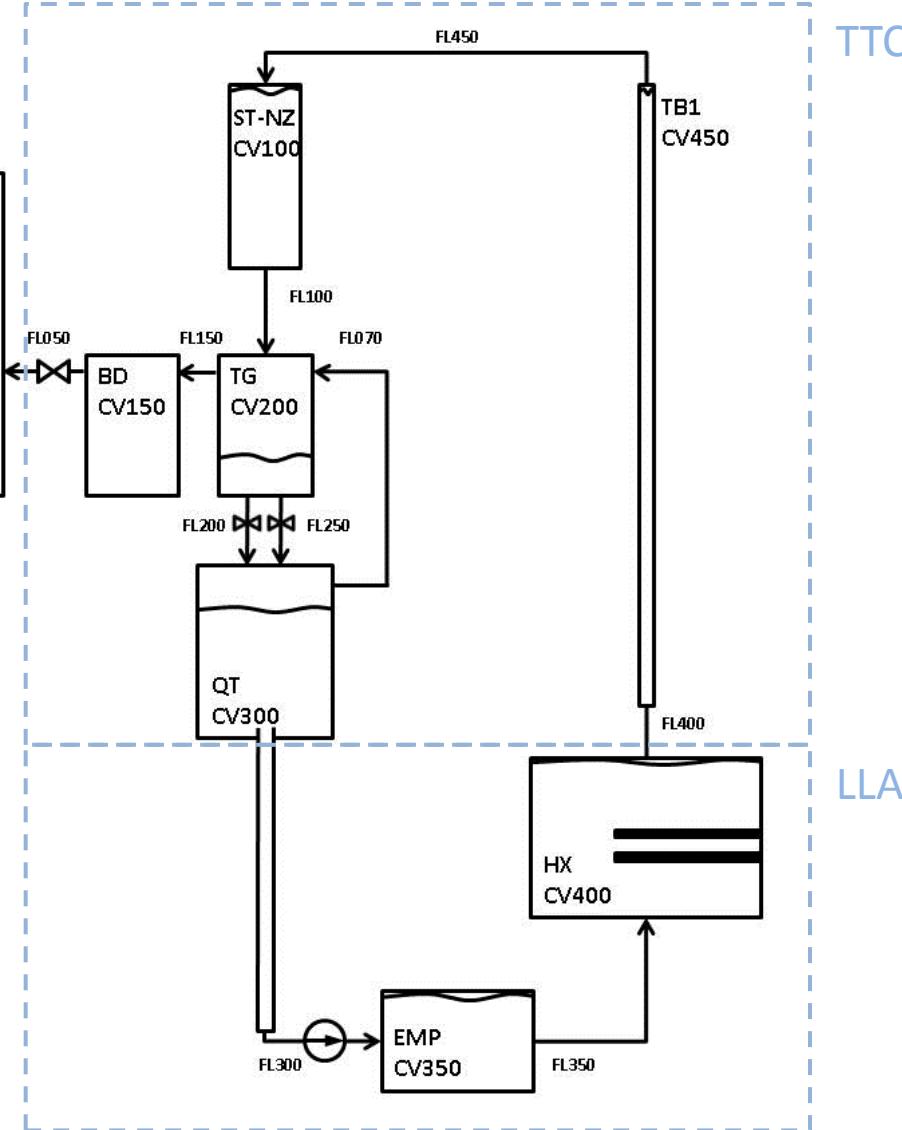
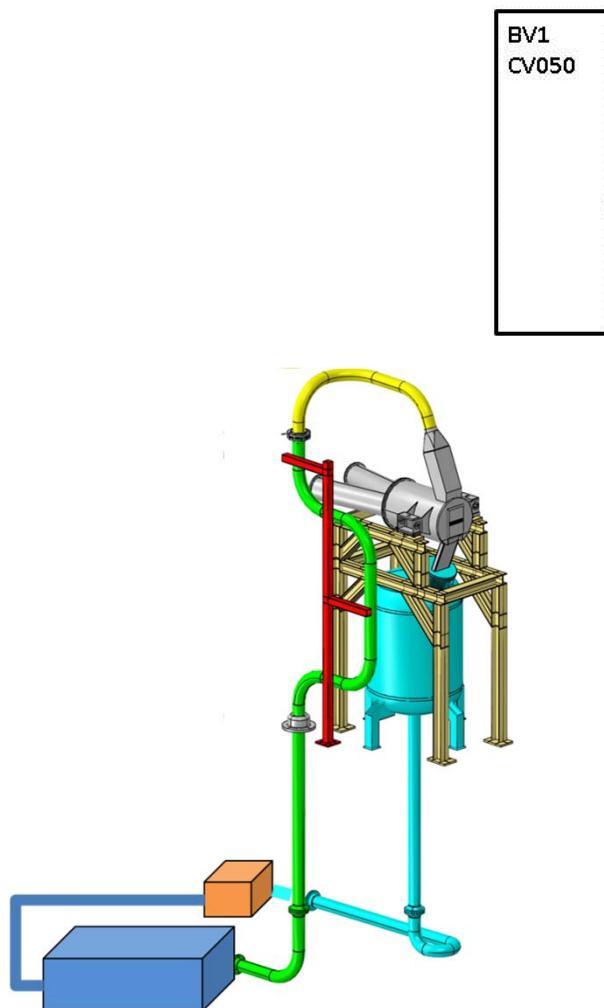


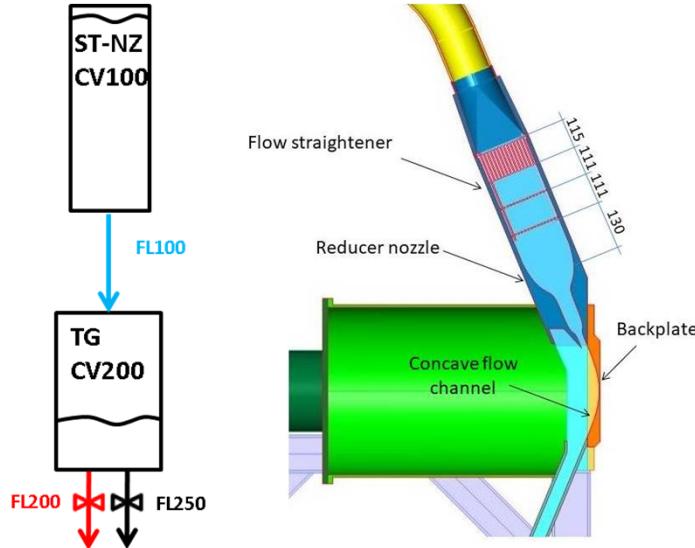
D. Bernardi. IFMIF-DONES Target System Design Description Document. EFDA_D_2N74W4 (2017).

Li Loop Modeling



Basic model
for Melcor-fusion





Key phenomenology: Li flows at high velocity in a small thickness layer (25 mm) to remove the high local power (5MW)

- A specific CVH/FL model is considered (“Momentum flux” option has been first explored without success)

Mass flow rates of FL100 & FL200 are coupled by CF420 (same flow path area):

FL200T1 2 420

*

CF42000 VELFLOW multiply 3 1.0 0.0

CF42010 1.0 0.0 FL-VELLIQ.100

CF42011 1.0 0.0 CVH-RHOP.100

CF42012 1.0 0.0 CFVALU.419

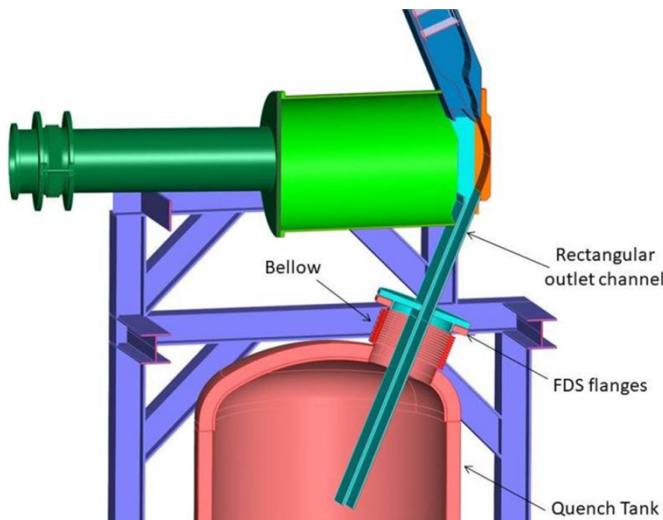
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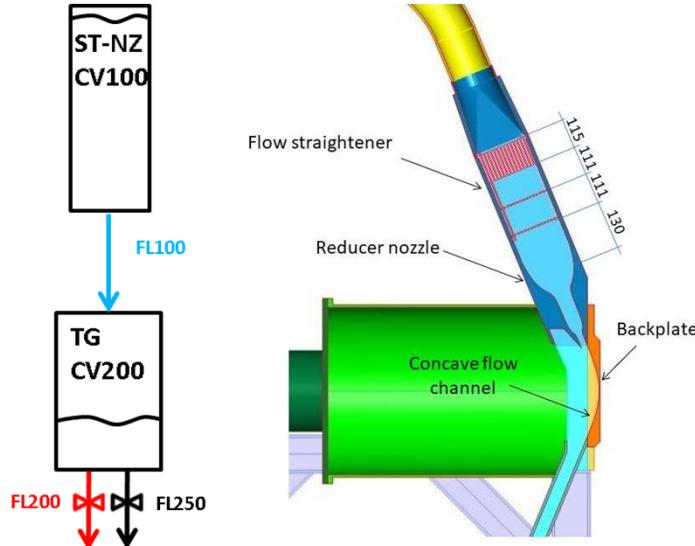
CF41900 INVRHO DIVIDE 2 1.0 0.0

CF41910 1.0 0.0 CVH-RHOP.200

CF41911 0.0 1.0 TIME

$$\frac{(\rho * v)_{fl100}}{\rho_{fl200}} = v_{fl200}$$





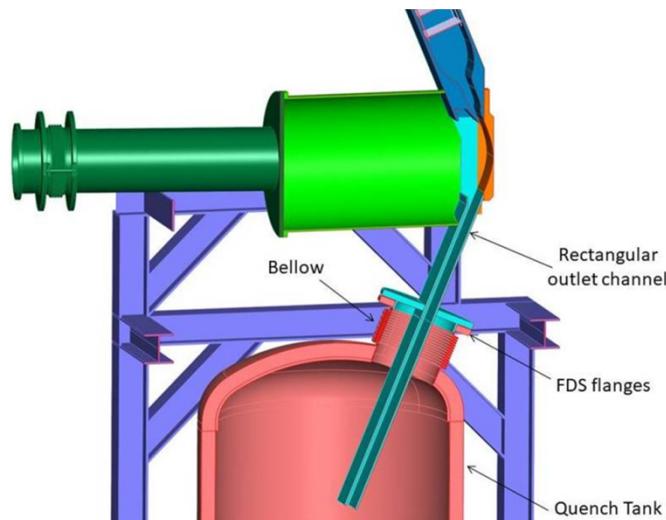
But...

- When CV100 runs out of Li (**FL-VELLIQ.100 = FL-VELLIQ.200 = 0 m/s**), there is still a little amount of Li mass in CV200

CV200 must be empty!

How to solve this issue?

- We created another flow path **FL250** (identical to **FL200**), which opens when velocity in **FL100** becomes zero, and
- We imposed a constant velocity for **FL250** equal to the last non-zero value of **FL-VELLIQ.200** until CV200 empties (*conservative assumption*)

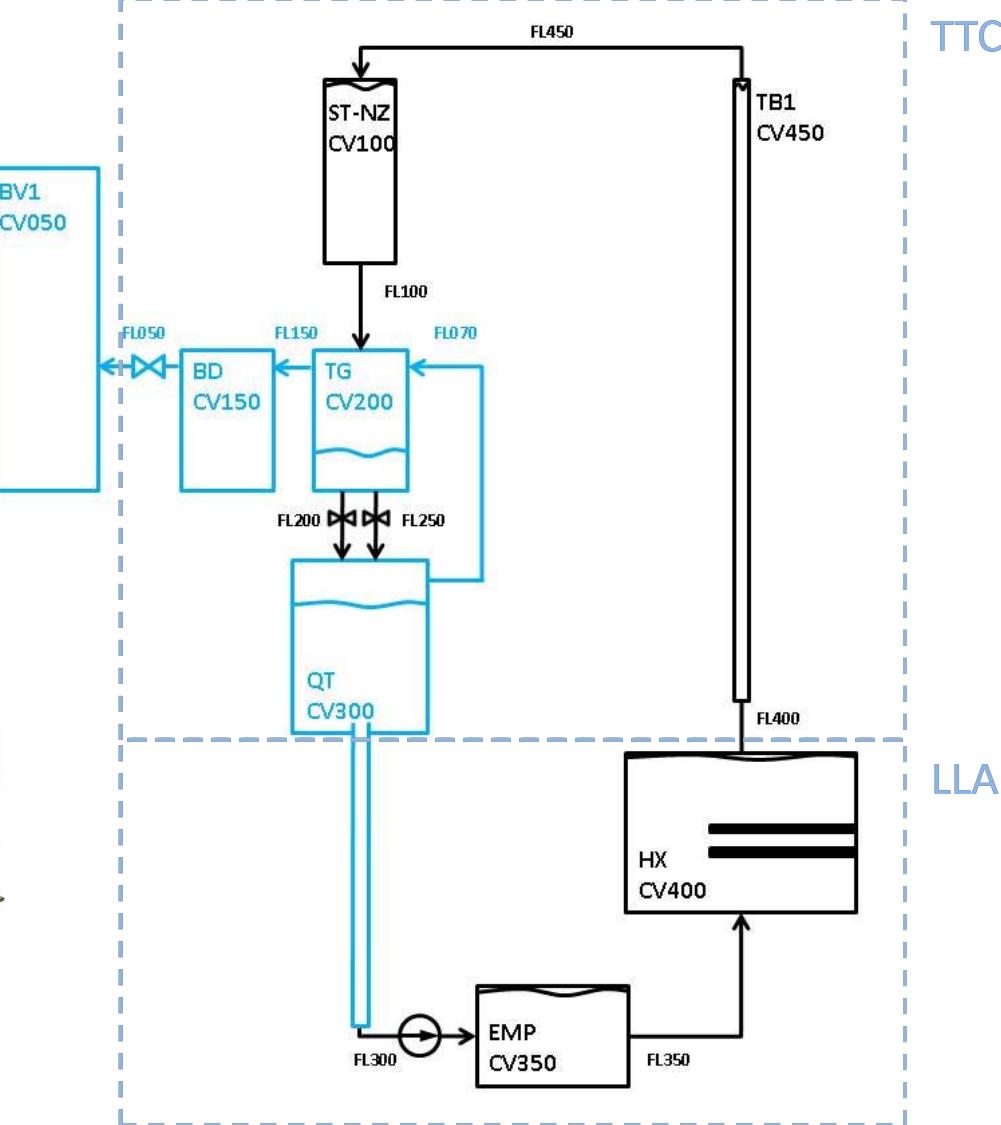
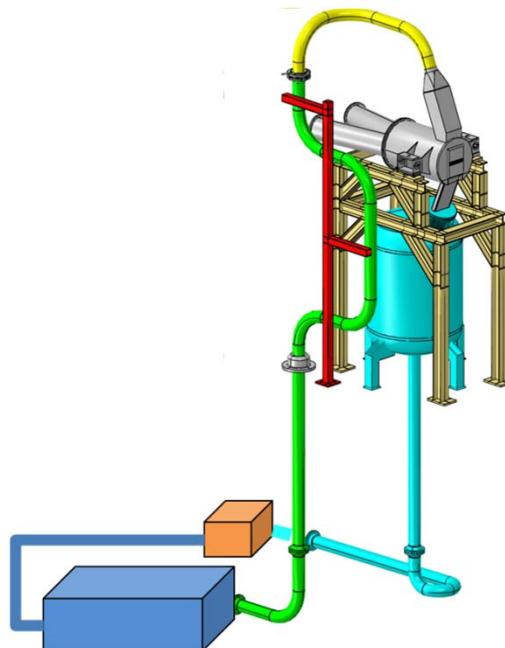


Li Loop Modeling



Basic model
for Melcor-fusion

“Vacuum pumping “
Low P, 1E-5 Pa
Boundary Volume

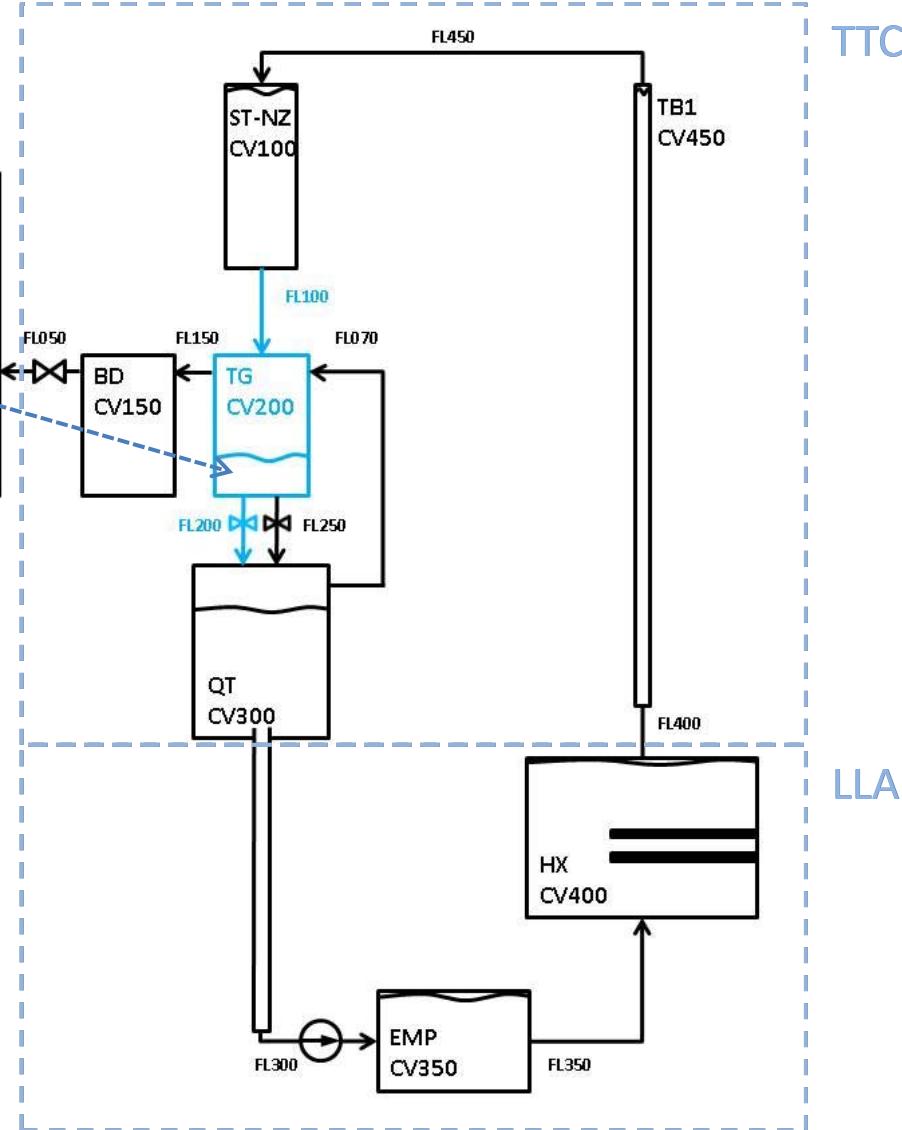
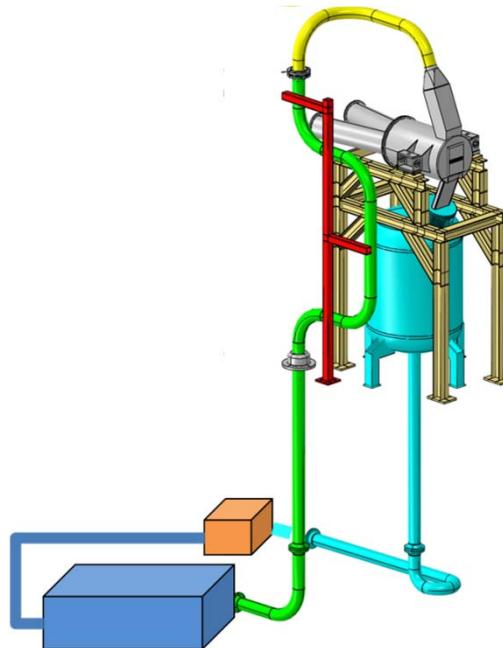


Li Loop Modeling



Basic model
for Melcor-fusion

- FL100-FL200 coupled
- 5 MW in little mass amount (<10 kg)

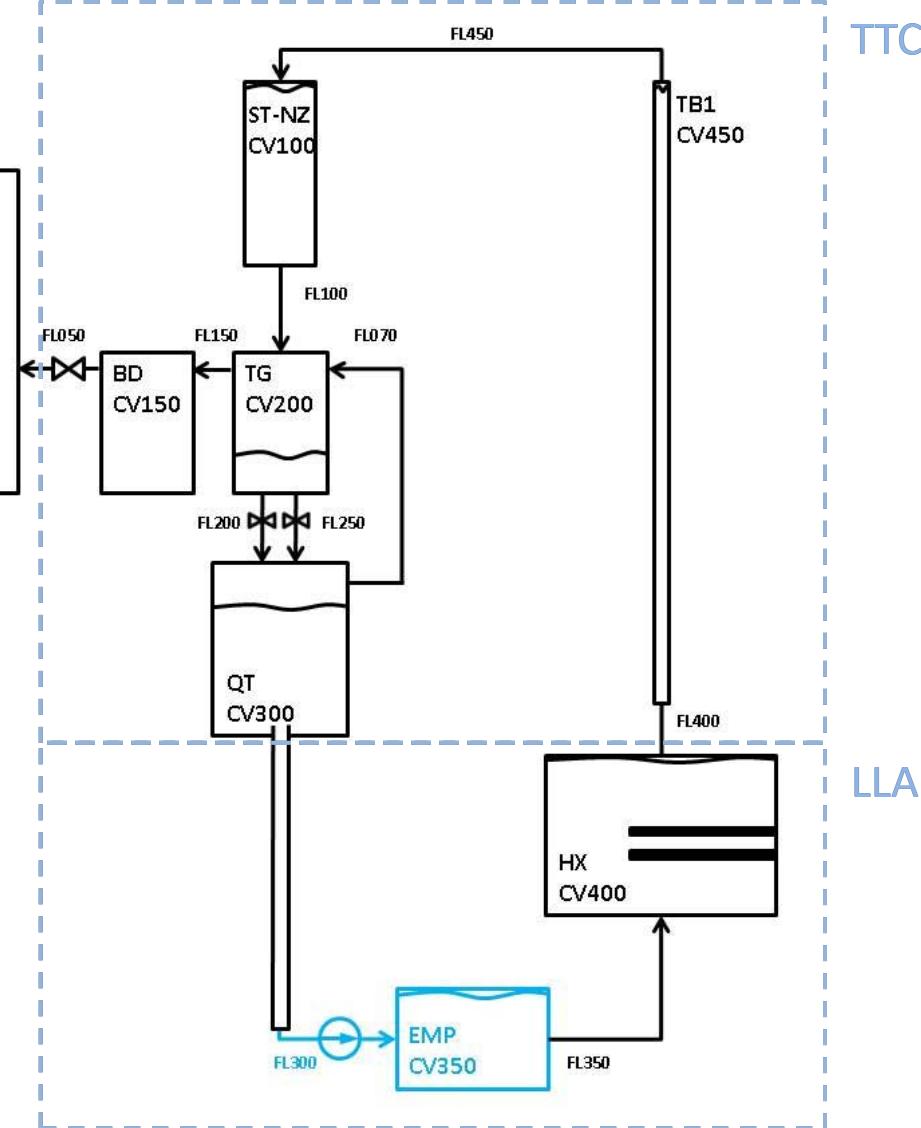
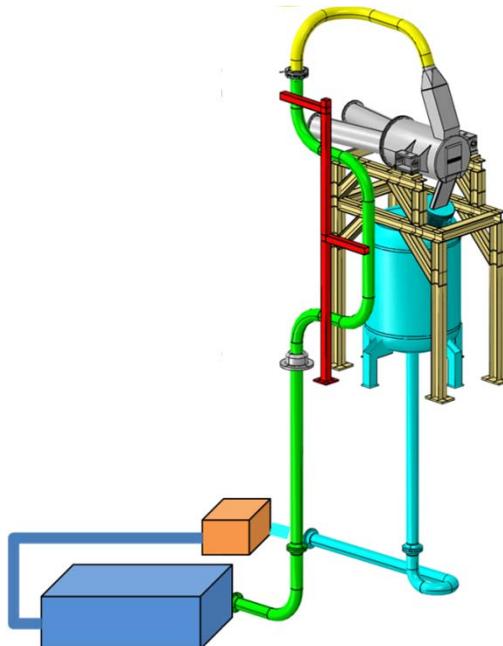


Li Loop Modeling



Basic model
for Melcor-fusion

Pump homologous
model

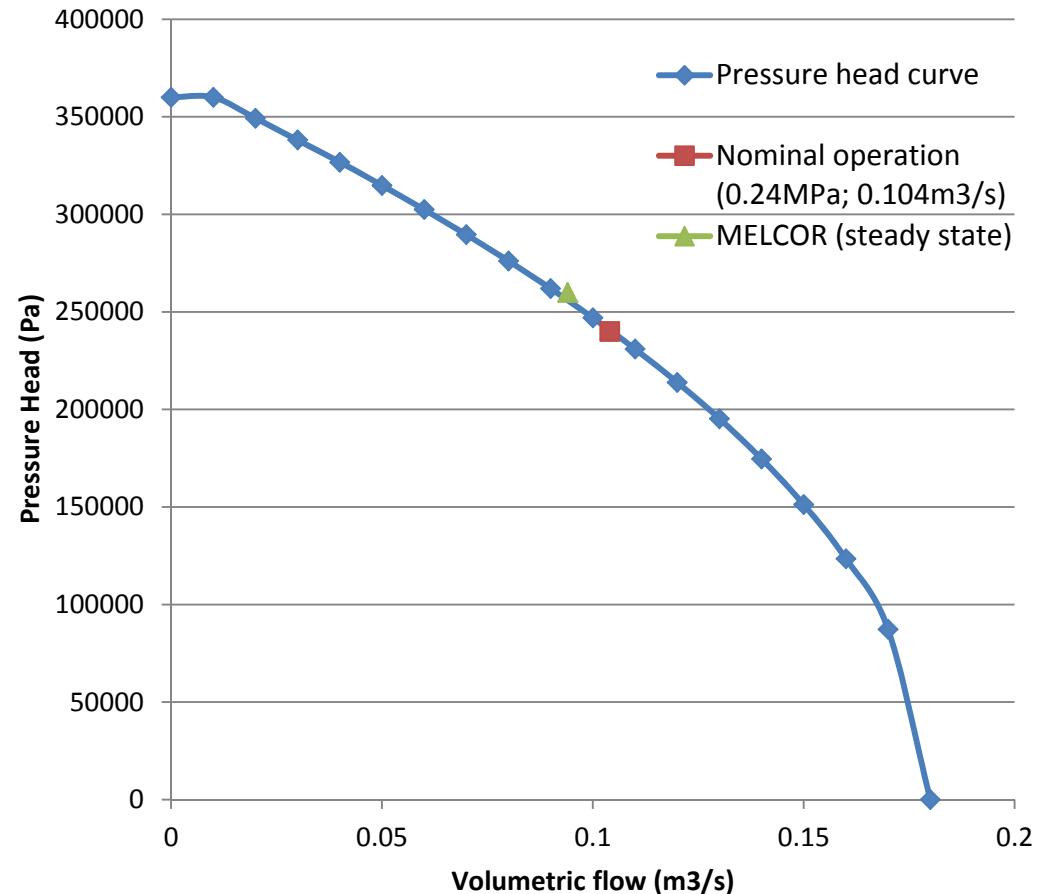


MELCOR “FANA” model (constant-speed coolant pump)

*MELGEN input

```
FL300P1   FANA   360000.0  0.18  0.01  550
*
*
CF55000   pump    TAB-FUN   1     1.0
CF55003   300
CF55010   1.0  0.0  time
*
TF30000   TAB300  3     1.0  0.0
*
*      TIME  Pressure head (Pa)
*
TF30010   0.0     1.0
TF30011   1500.00  1.0
TF30012   1510.0   0.0
```

**Pump
coastdown
(linear ramp)**



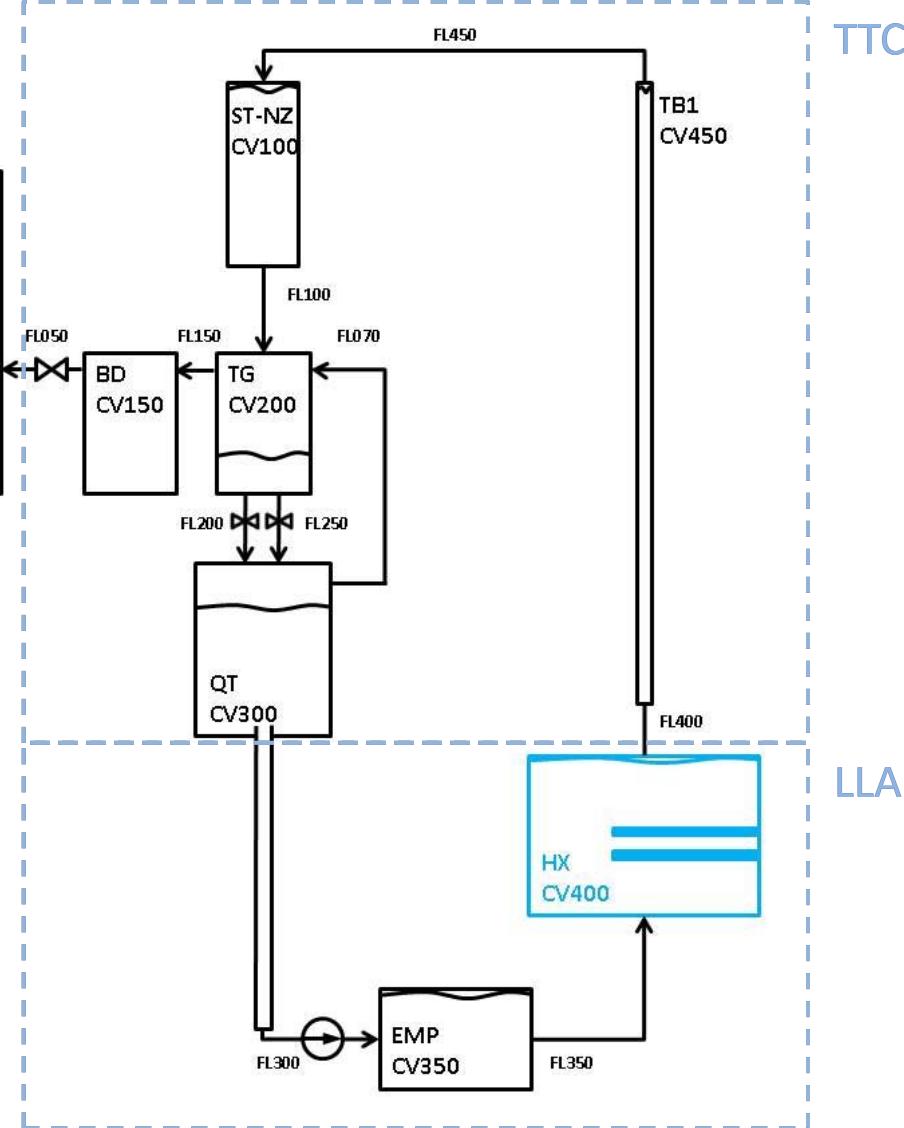
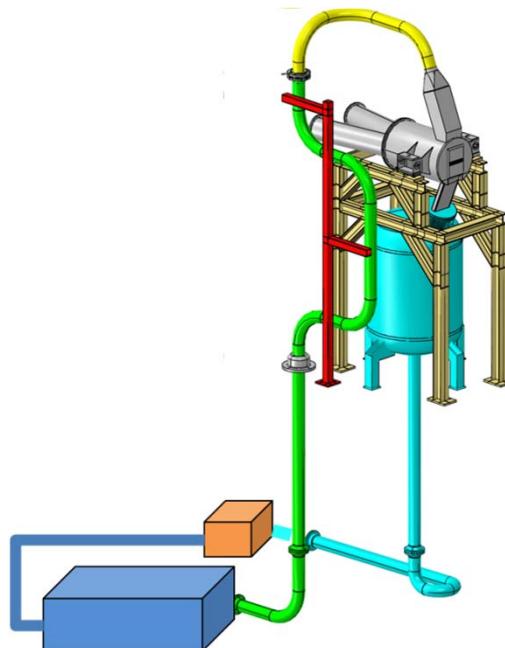
Pump curves to be explored!

Li Loop Modeling



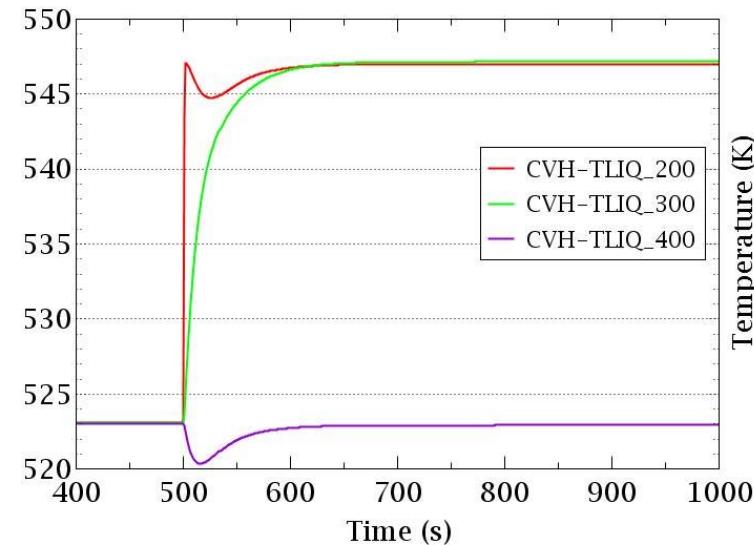
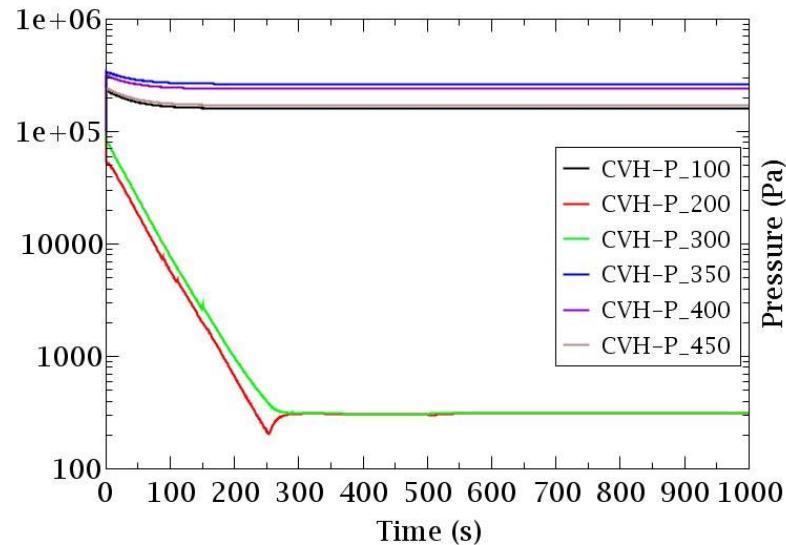
Basic model
for Melcor-fusion

HS at 245.5 °C



Start-up transient sequence

A steady state is achieved by means of an operational start-up transient



Steady state results ($t = 1000$ s) with power injection at $t=500$ s

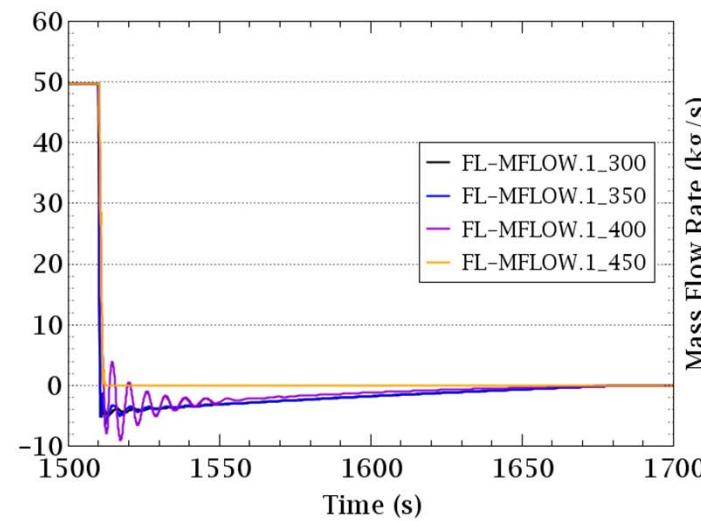
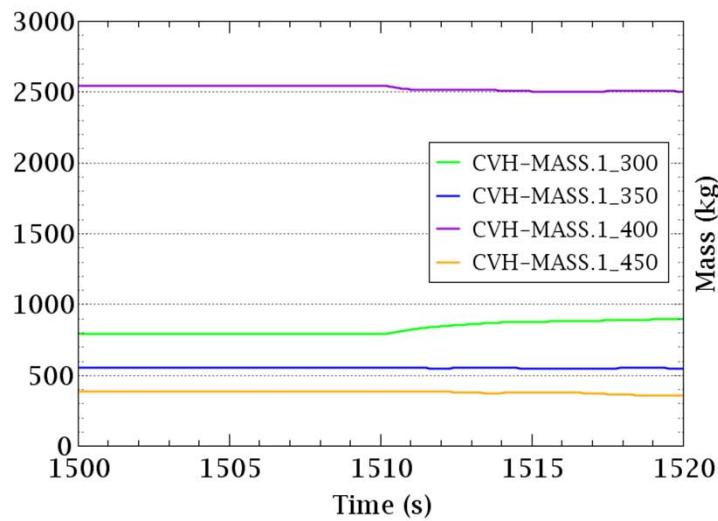
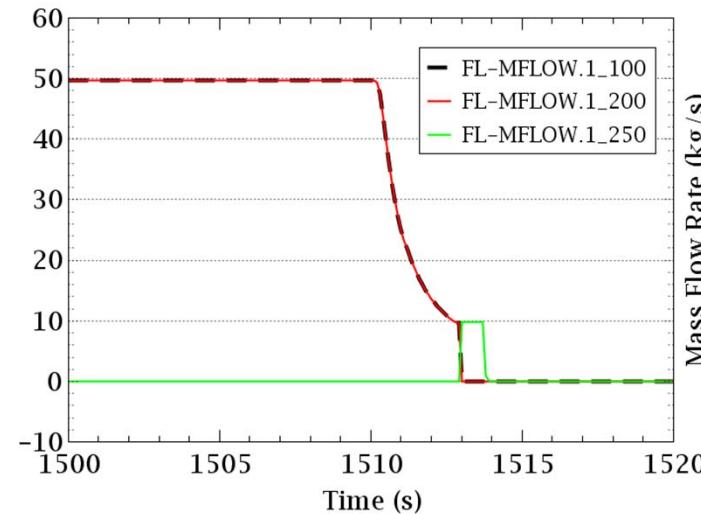
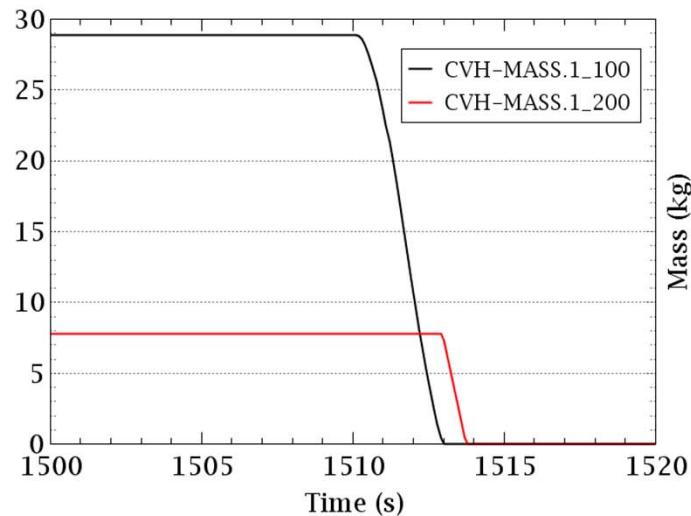
Parameter	Calculation	Reference	Comments
Pressure target	300 Pa	1E-3 Pa	<u>Not allowed below 200 -100 Pa range due to problems with Li EOS extrapolation</u>
Total circuit pressure loss	2.6E5 Pa	2.4E5 Pa	Curve pump is unknown; here is fitted for desired point
Total Li mass flow rate	49.7 kg/s	49.7 kg/s	Same comment
Velocity at nozzle exit	15 m/s	15 m/s	Li target flow velocity between 10-15 m/s (in operation)
Li temperature in HX	250 °C	250 °C	
Li temperature in QT	274 °C	274 °C	
Total Li volume in the loop	8.45 m3	8.44 m3	Li volume of the impurity reduction system is not considered

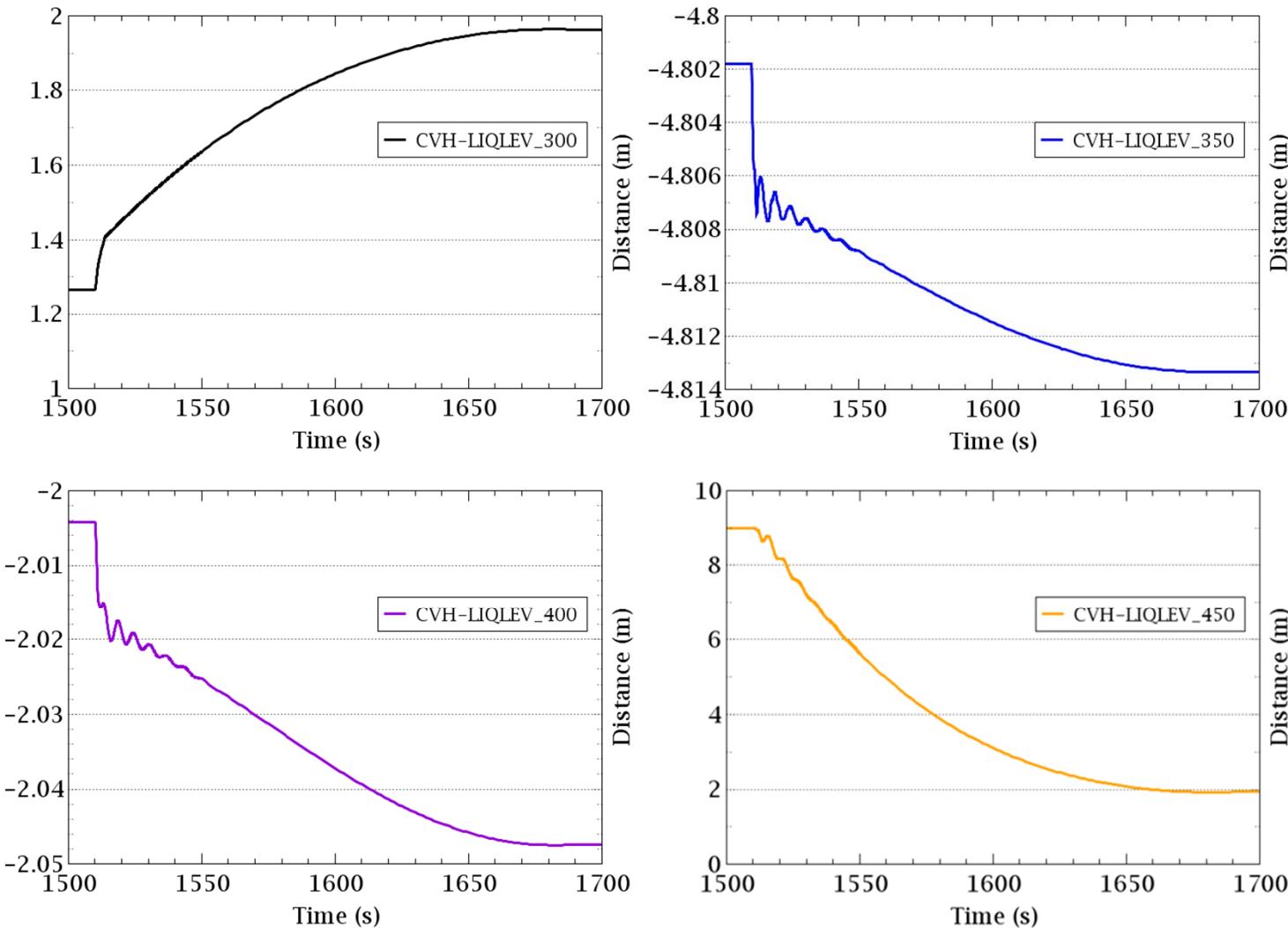
Potential consequences of a LOFA scenario:

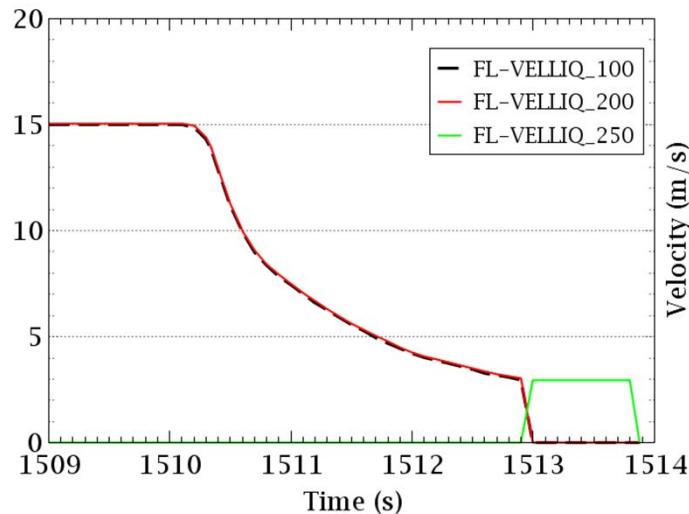
- **Backplate thermal overload and rupture** (if beam is not promptly stopped)
- **Release of Li and its radioactive impurities** into Target Test Cell (TTC) or Li Loop Area (LLA) with direct increase of ORE
- Possible **Li-air and/or Li-vapor reactions** (if inert atmosphere is not guaranteed inside TTC or LLA)

Main events of MELCOR transient sequence:

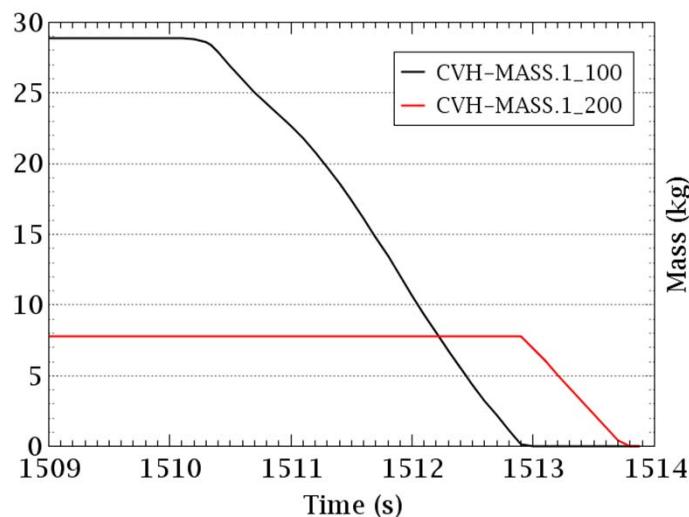
Event	Time (s)	Quantity
Start of calculation (pump on)	0	
Power injection into target (\rightarrow Li mass)	500	5 MW
Pump trip (pump head linear ramp to zero)	1500-1510	<i>assumed</i>
Li mass flow rate reaches 70% of its nominal value in the target (<i>assumed</i>)	1510.7	$\sim 35 \text{ kg/s}$
Beam shutdown ($5 \rightarrow 0 \text{ MW}$ in 1s)	1510.7 – 1511.7	<i>assumed</i>
Target completely empties	1513.9	-
End of calculation	3000	-

MELCOR results (Li mass flow rates and Li mass inventories)

MELCOR results (Li mass elevations in CVs)

MELCOR results (Li flow velocities and mass inventories)

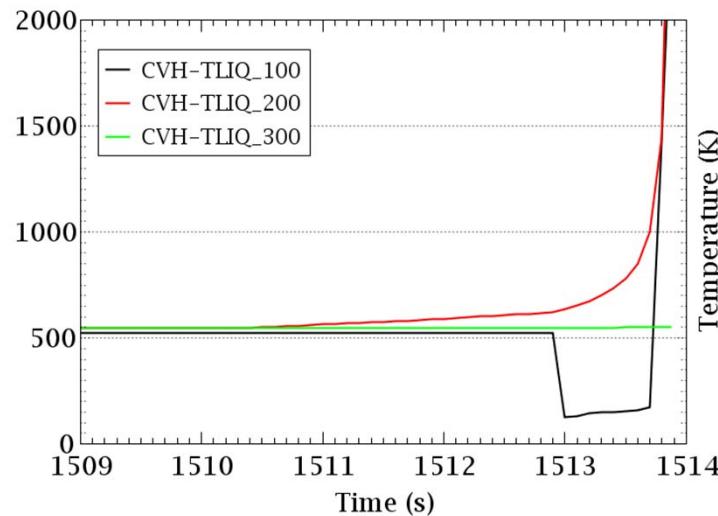
- Li flow velocities and mass inventory evolutions inside CV100 & CV200 show a very similar tendency with their respective quantities of the previous scenario



- CV200 empties at $t = 1513.9$ s
- Time range available to shut down the beam and to prevent damages to the backplate and surrounding structures is ~ 14 s from the beginning of the pump trip

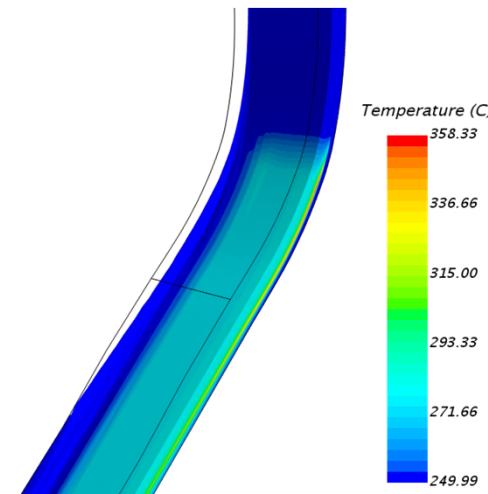


MELCOR results (Li temperature in CV100, CV200 & CV300)



- Temperature in CV200 (Li target) raises from 547 to 2000 K in less than 4 seconds from $t = 1510$ s (when pump head becomes zero)!

CFD simulation of Li jet temperature distribution (DONES: 5 MW, 15 m/s)

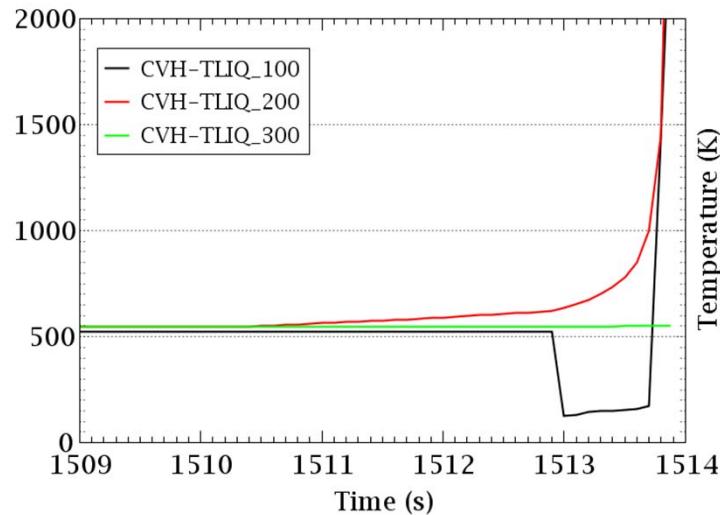


$T_{max} = 358^{\circ}\text{C}$ (631 K) (in the Li bulk)
 $T_{boil} \sim 1030^{\circ}\text{C}$ (1303K)
 $\Delta T \sim 672^{\circ}\text{C}$

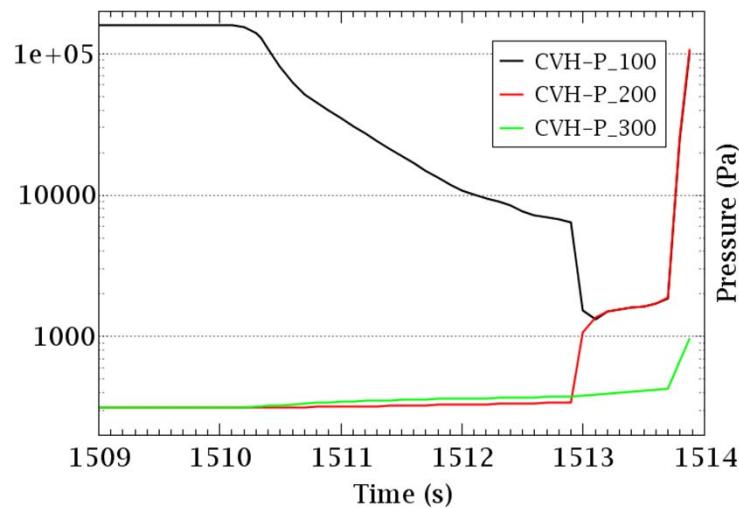
S. Gordeev. Preliminary Numerical Analysis of Li jet, BP Discharge Line and QT, with power deposition. EFDA_D_2N4NNF v1.1 (2017).

$T_{surf} = 278^{\circ}\text{C}$ (551 K) (at Li-free surface)
 $T_{boil} \sim 342^{\circ}\text{C}$ (615 K)
 $\Delta T \sim 65^{\circ}\text{C}$

S. Gordeev. Evaluation of Li Vaporization in the TA. EFDA_D_2MNNTD v1.1 (2017).

MELCOR results (Li temperature and pressure evolution in CV100, CV200 & CV300)

- Temperature in CV200 (Li target) raises from 547 to 2000 K in less than 4 seconds from $t = 1510$ s (when pump head becomes zero)!



- Atmospheric pressure is reached inside CV100 & CV200 at the end of the calculation

Final remarks



❑ A preliminary model for DONES Li loop is available

- Good agreement between MELCOR predictions (steady state) and reference design requirements has been achieved
- First simulations of LOFA scenario have been performed

❑ Not straightforward modeling

- High sensitivity to adopted nodalization
- Numerical problems experienced:
 - Dependence on timestep
 - EOS impact when extrapolation at low pressures

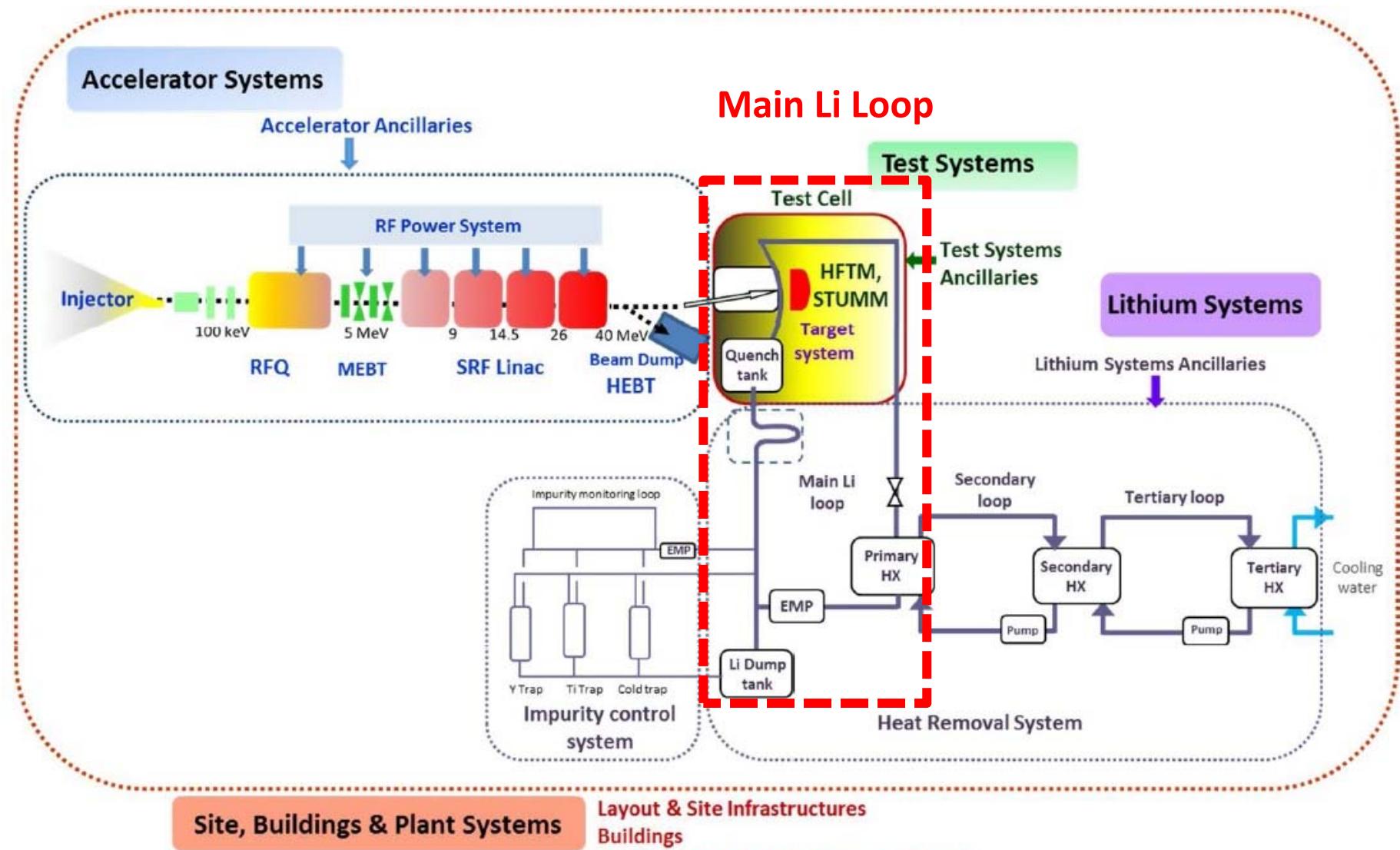
❑ Future developments and exploratory calculations

- Modeling upgrade based on future design documents
- Sensitivity to
 - HS implementation for all control volumes
 - Pump coastdown curve for design improvement (coastdown tail)
 - New model for Li target
 - ...
- Simulation of LOCA scenarios in TTC and LLA (candidates for DONES “RAS”) with release of Li radioactive impurities (tritium, activation products)

Thank you for your attention

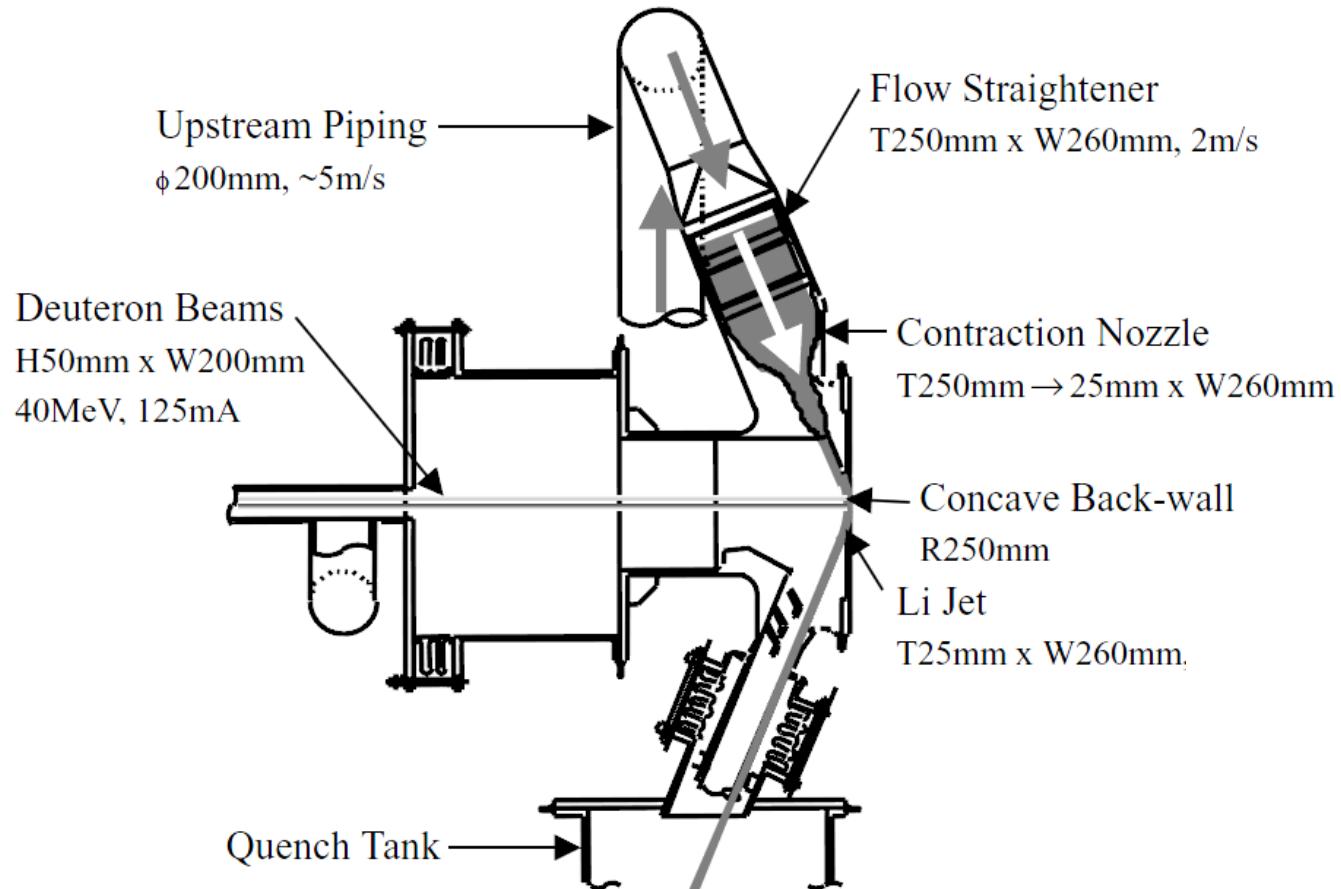
Questions? Comments? Suggestions?

DONES Plant Configuration



Backup slides

Cross-sectional schematic of DONES target assembly



Backup slides

Li Loop total pressure loss (estimated)

Element	No.	Specification	Pressure loss [kPa]
Pipe, in TC	1	6B, Sch40, 13.24 m	11.16
Pipe, EMP - LLA ceiling	1	8B, Sch20, 36.48 m	6.88
Pipe, QT - EMP	1	10B, Sch20, 17.89 m	1.15
Bend, in TC	2	6B, 90°, R228.6 mm	3.60
Bend, EMP - LLA ceiling	17	8B, 90°, R304.8 mm	9.35
Bend, QT - EMP	6	10B, 90°, R381.0 mm	1.32
Gate valve, under QT	1	10B (loss coefficient: $\zeta = 0.05$)	0.05
Globe valve	1	CV408 (6B)	57.66
QT outlet	1	ID: 254.4 mm → 10B ($\zeta = 0.5$)	0.55
Primary HX	1	Li side: L7.15 m, ID1.1 m	17.00
Reducer, LLA ceiling	1	8B → 6B, L152.4 mm	0.10
Flow straightener	1	-	15.7
Double reducer nozzle	1	L370 mm, W260 mm, T200 → 62.5 → 25 mm	75.1 ~46%
Total pressure loss			199.61
Head, inlet pipe - Li level in QT		8.13 m	40.16
Pressure loss + head			239.77

Li conditions for pressure loss estimation

Item	Value
Li flow rate	0.104 m ³ /s (16 m/s at nozzle exit)
Li temperature	250°C
Li density	510 kg/m ³
Li kinematic viscosity	9.83E-7 m ² /s