



Insights on an SBO accident in BWR

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I. Introduction

- **Framework**

- *Source term evaluation in a BWR SBO accident*

- **Objectives**

- *To explore the role played by suppression pool nodalization in the containment thermal-hydraulics*
- *To find a conservative scenario for FP release and source term*

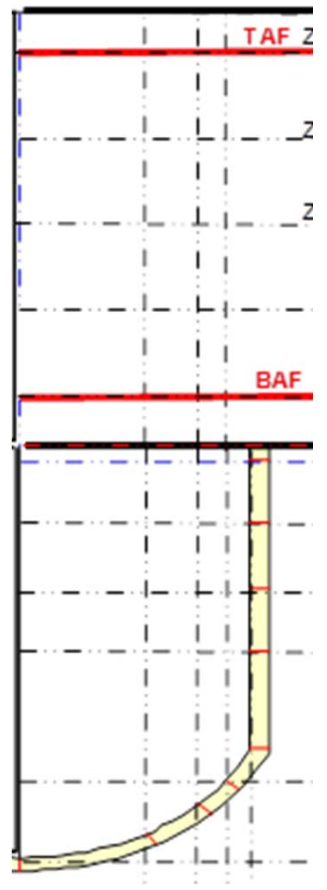
- **Scope**

- *MELCOR v2.1 analysis of a BWR3-Mark1 plant*

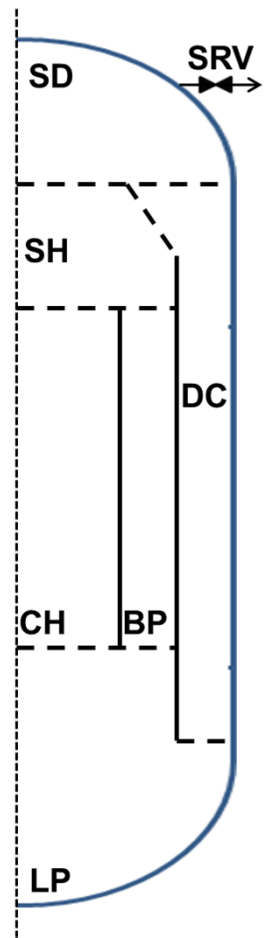


II. Plant modelling

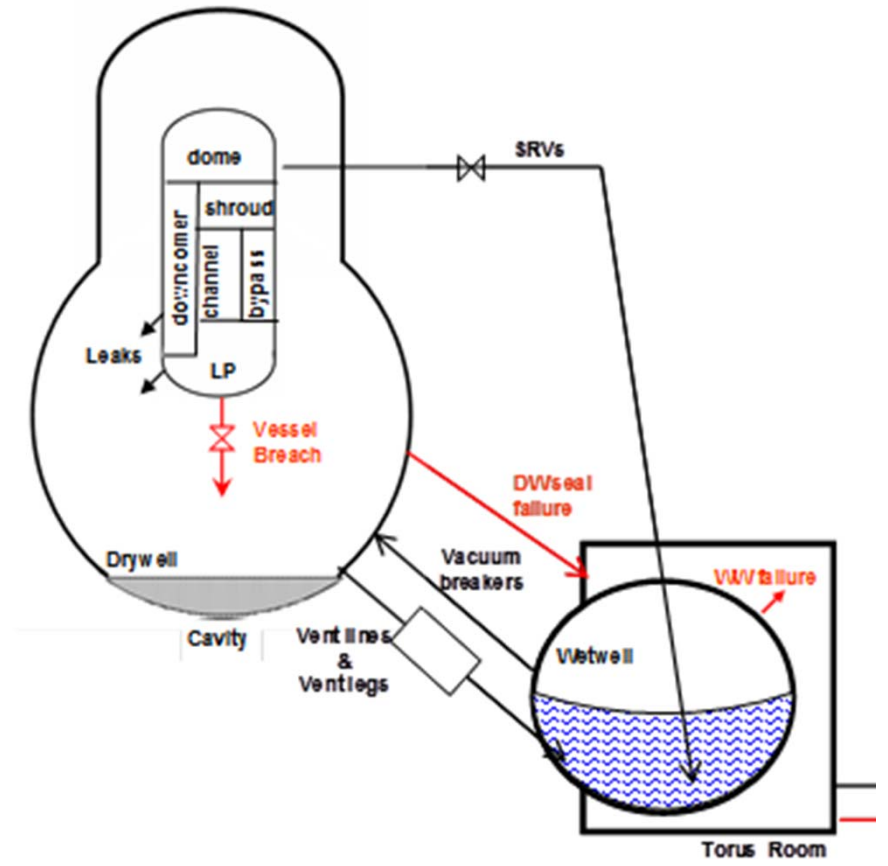
Core & LP



RPV



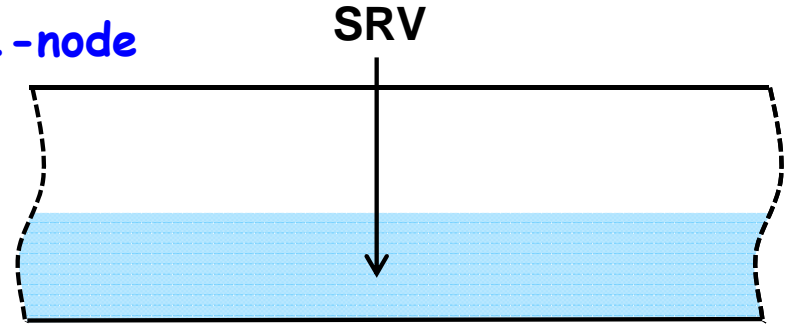
PCV



II. Plant modelling (wetwell)

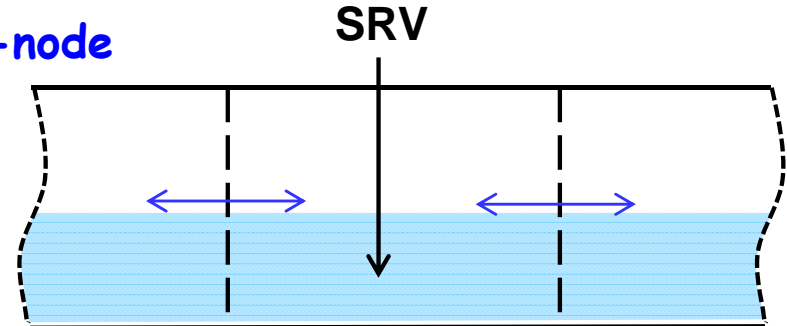
Azimuthal stratification

1-node



Perfect mixing

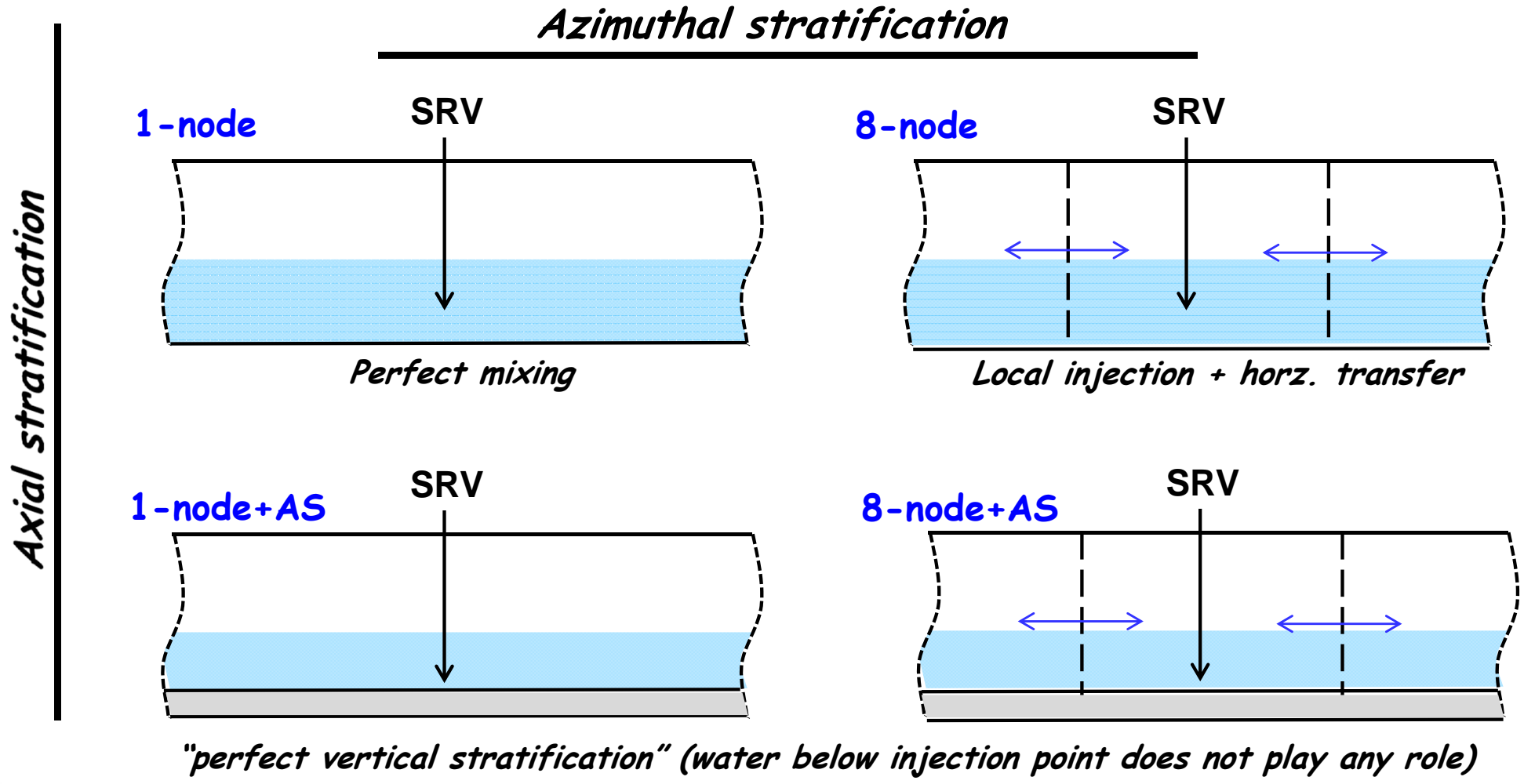
8-node



Local injection + horz. transfer



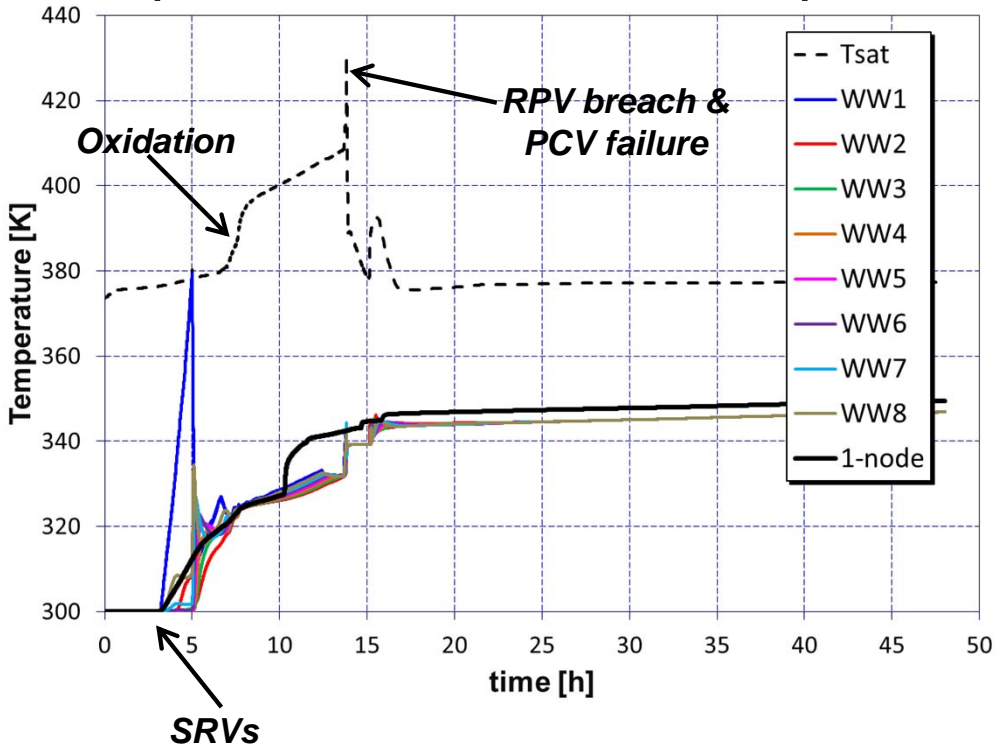
II. Plant modelling (wetwell)



III. Results: Thermal-hydraulics

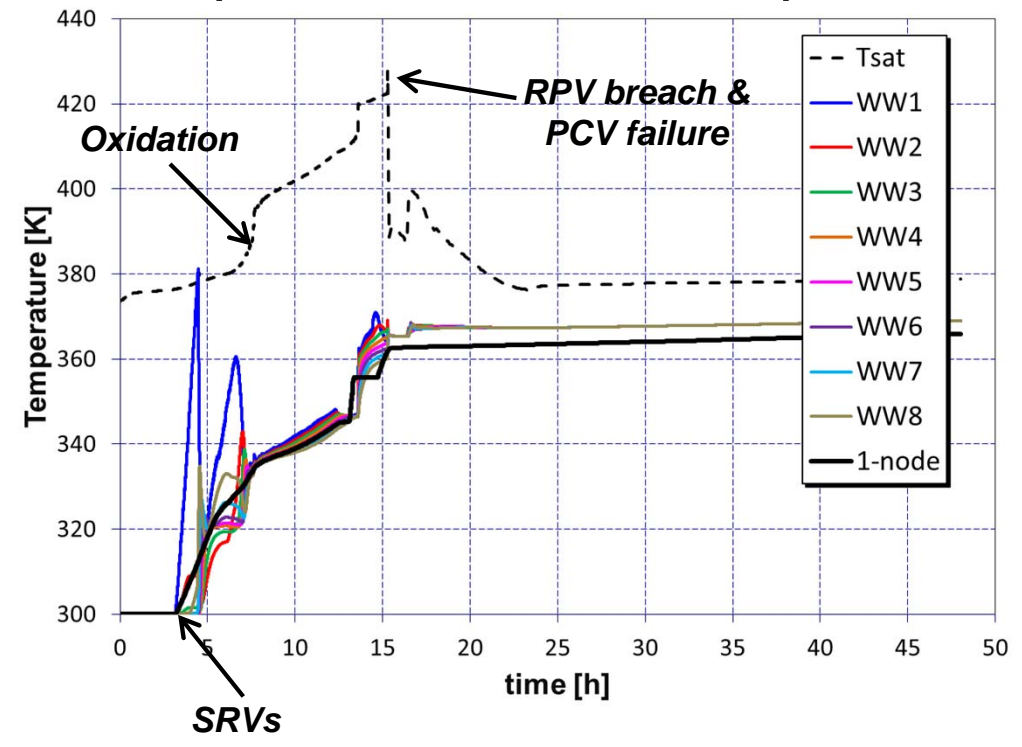
SP temperature

(without axial stratification)



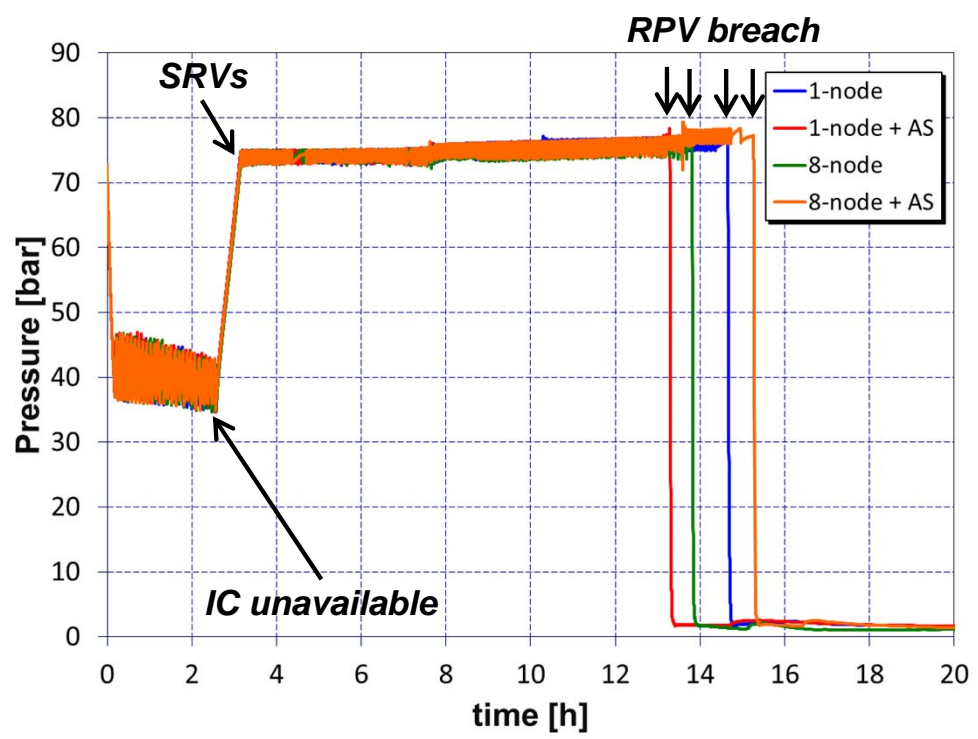
SP temperature

(with axial stratification)

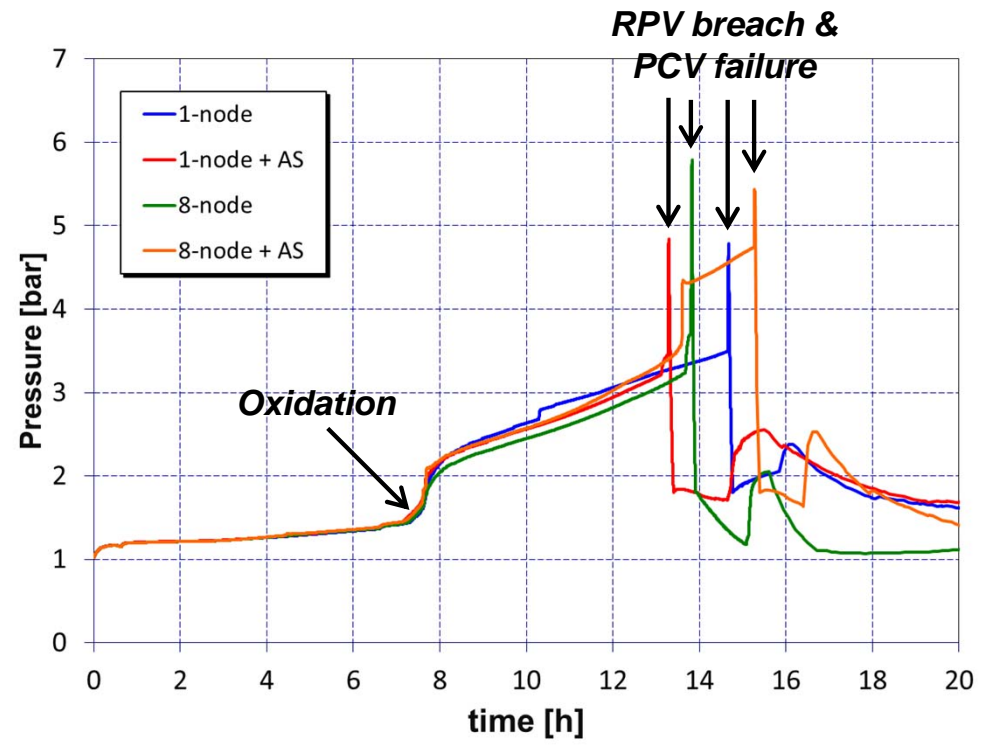


III. Results: Thermal-hydraulics

RPV pressure



PCV pressure



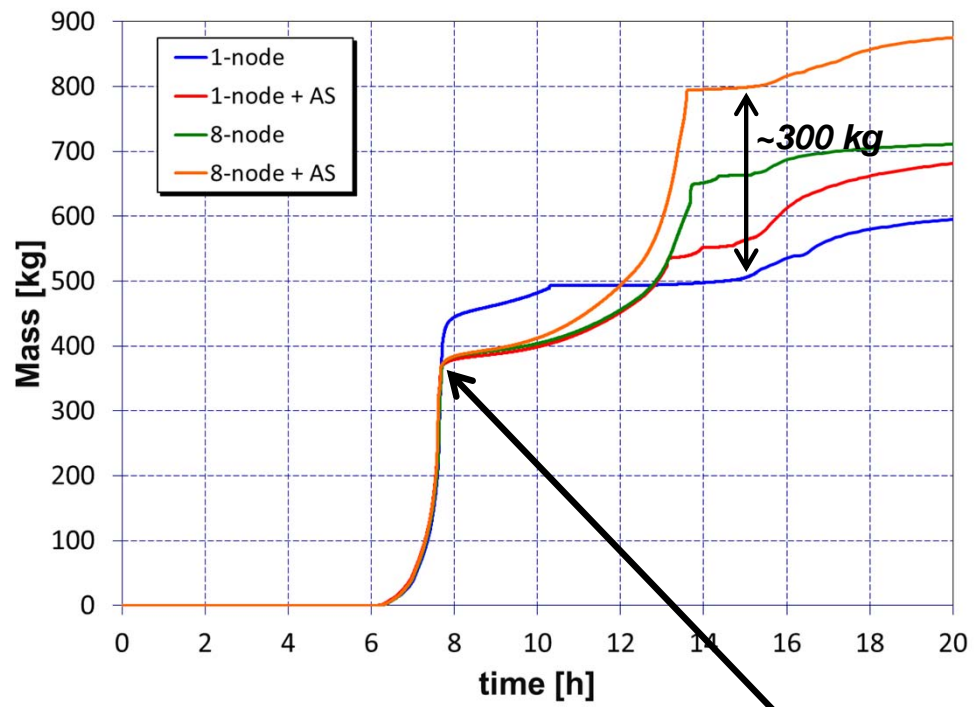
III. Results: Key event chronology

Key event	1n	1n AS	8n	8n AS
IC operation (h)	0-2.6	0-2.6	0-2.5	0-2.6
SRV operation (h)	3.2-14.2	3.2-13.3	3.2-13.8	3.2-14.7
Core uncover (h)	5.2-6.8	5.2-6.8	5.2-6.8	5.2-6.8
Fuel in LP (h)	10.3	13.1	13.6	13.5
Dry RPV (h)	11.9	13.3	13.8	14.7
RPV failure (h)	14.7	13.3	13.8	15.3
PCV failure (h)	14.7	13.3	13.8	15.3

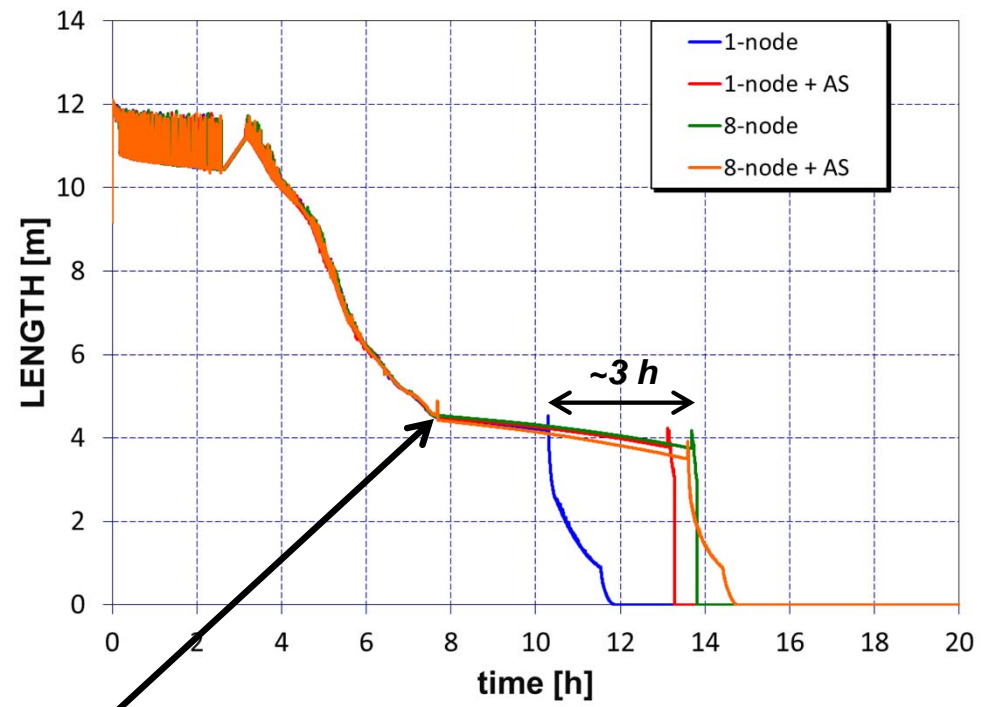


III. Results: In-vessel evolution

H₂ production



Water level

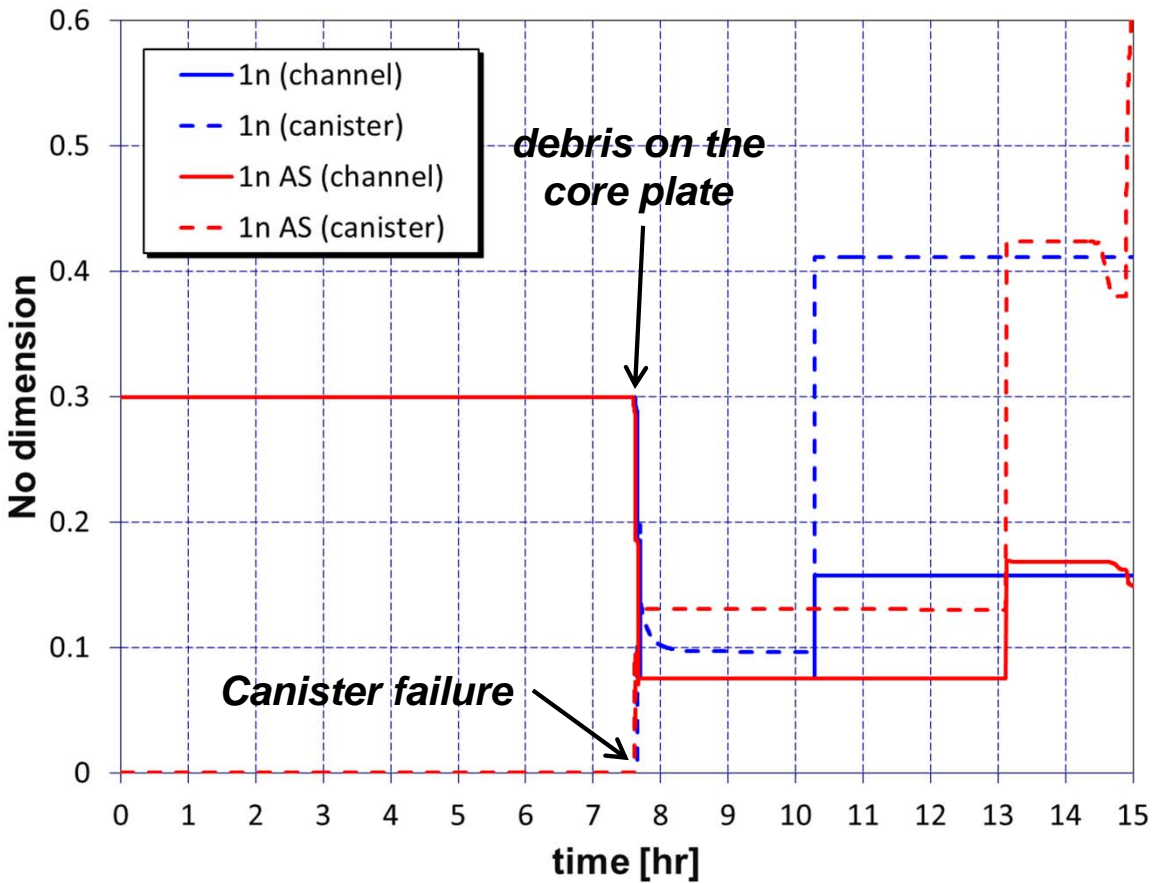


Differences originated at ~ 7.6 h



IV. In-vessel insights

Open fraction of flow paths



Comparison of cases

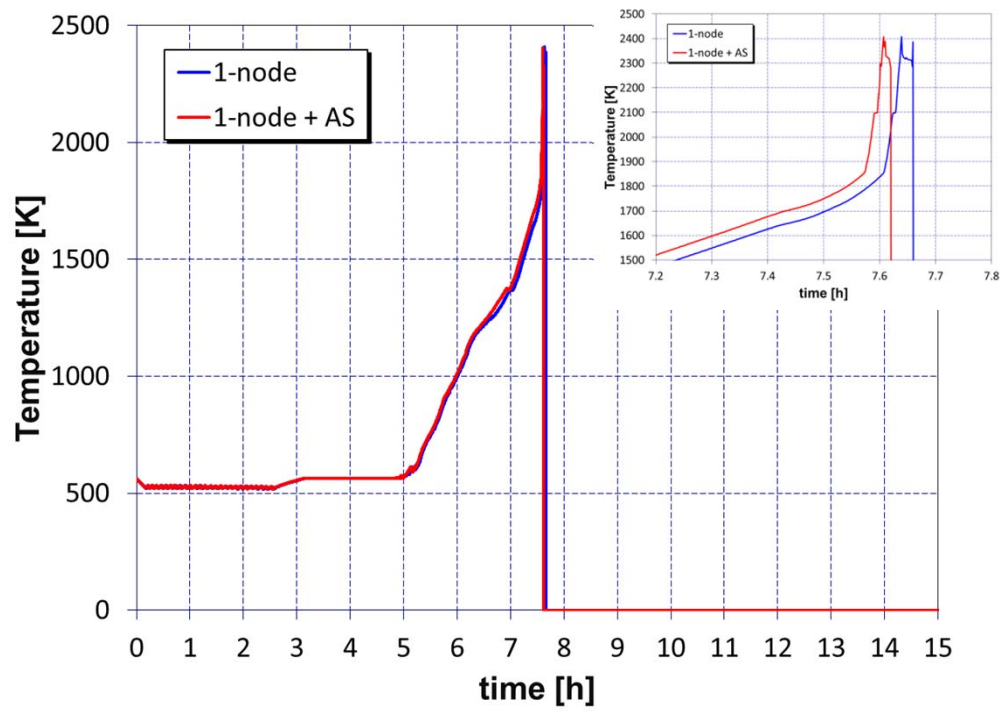
1-node vs 1-node + AS

- Failure cross section of canister has a difference ~25%

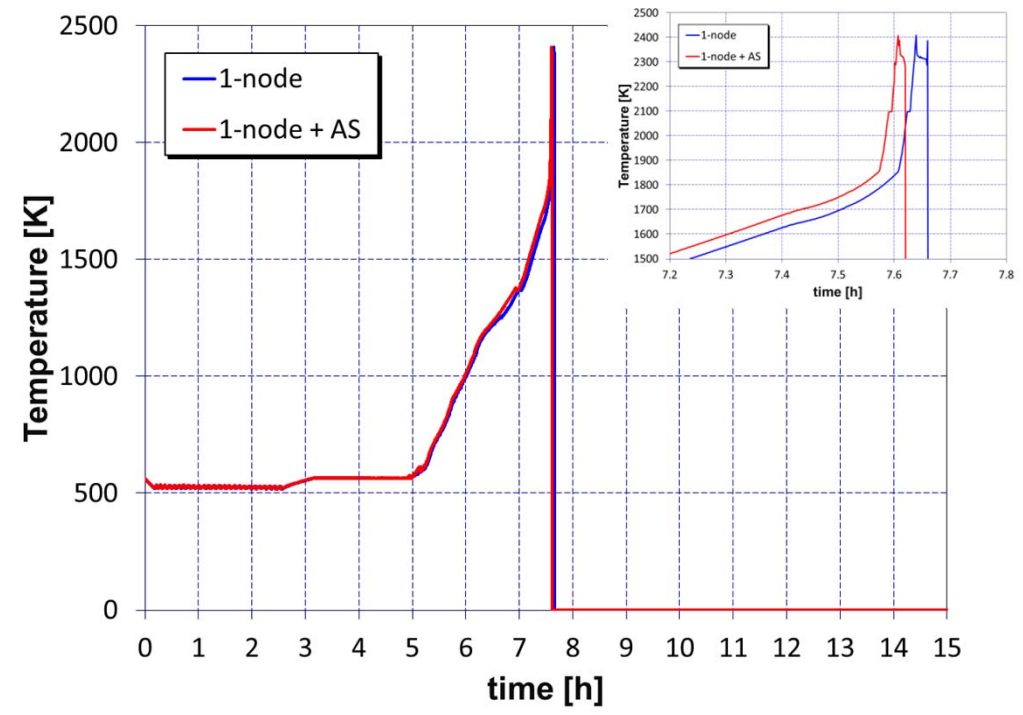


IV. In-vessel insights

Cladding temperature (central ring)



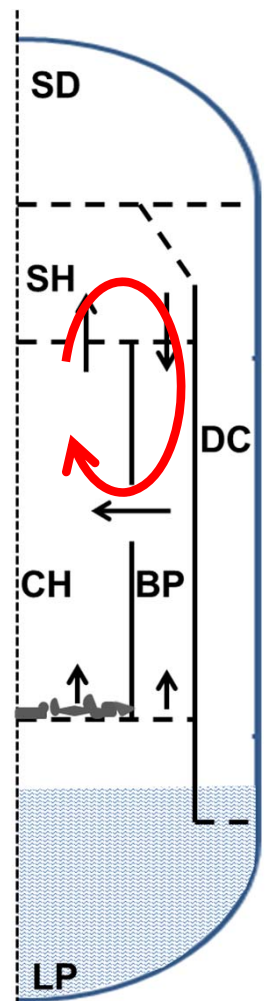
Canister temperature (central ring)



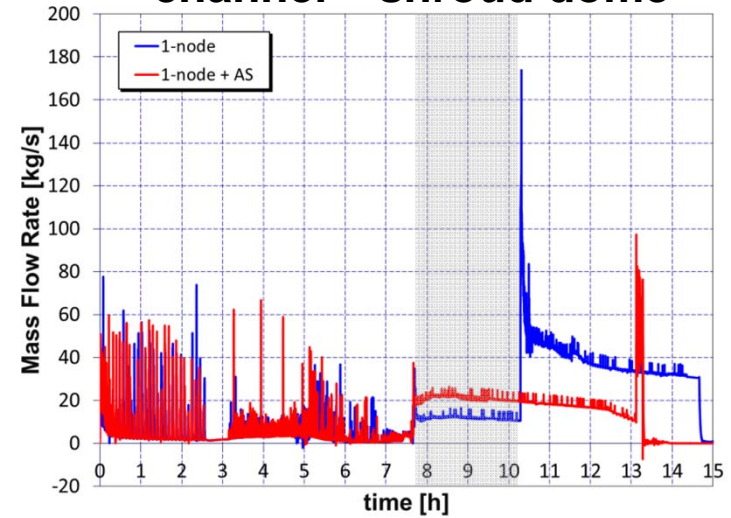
Insignificant differences in clad and canister temperature (~5 K and ~ 3 min)



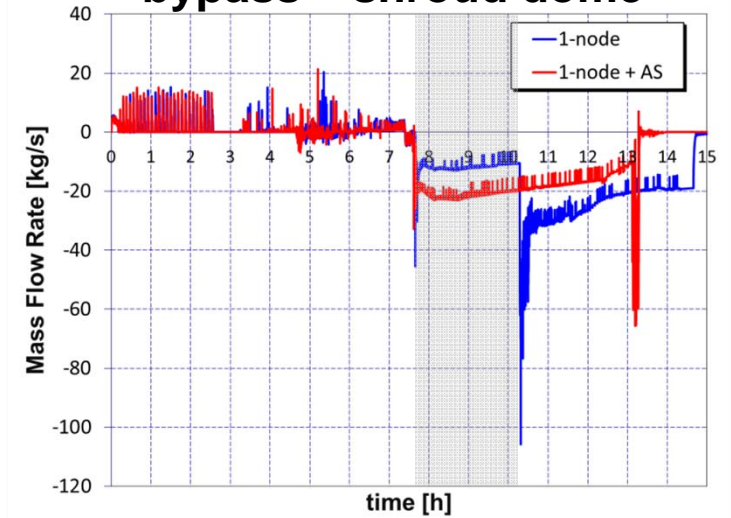
IV. In-vessel insights



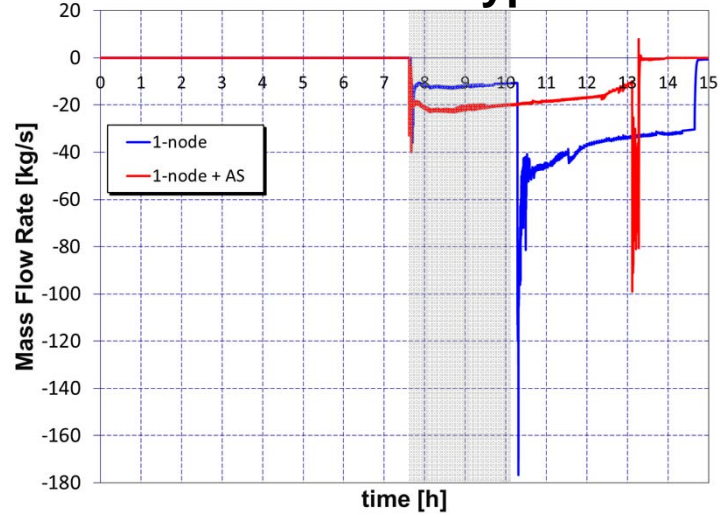
channel – shroud dome



bypass – shroud dome



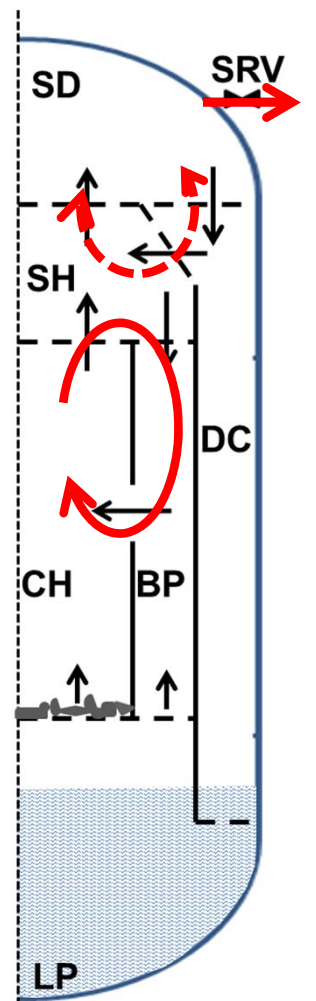
channel – bypass



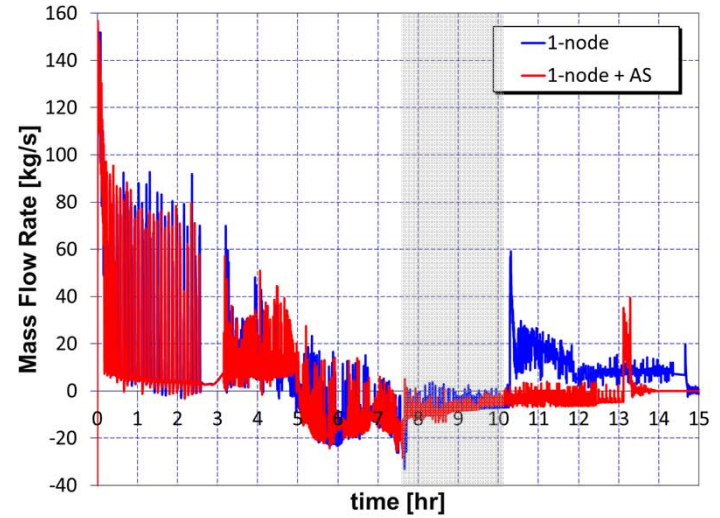
- A convective flow loop is developed in the core region when canister fails
- Case '1-node' has lower mass flow rate through the channel (*lower CH-CP cross section*)



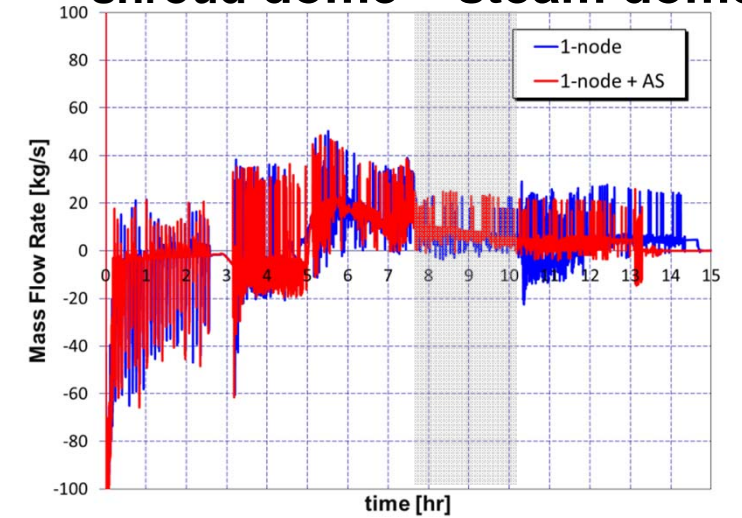
IV. In-vessel insights



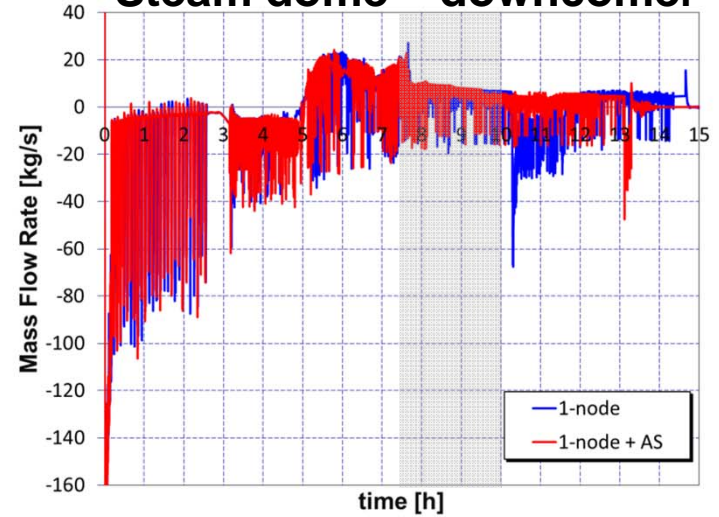
shroud dome – downcomer



shroud dome – steam dome



Steam dome – downcomer

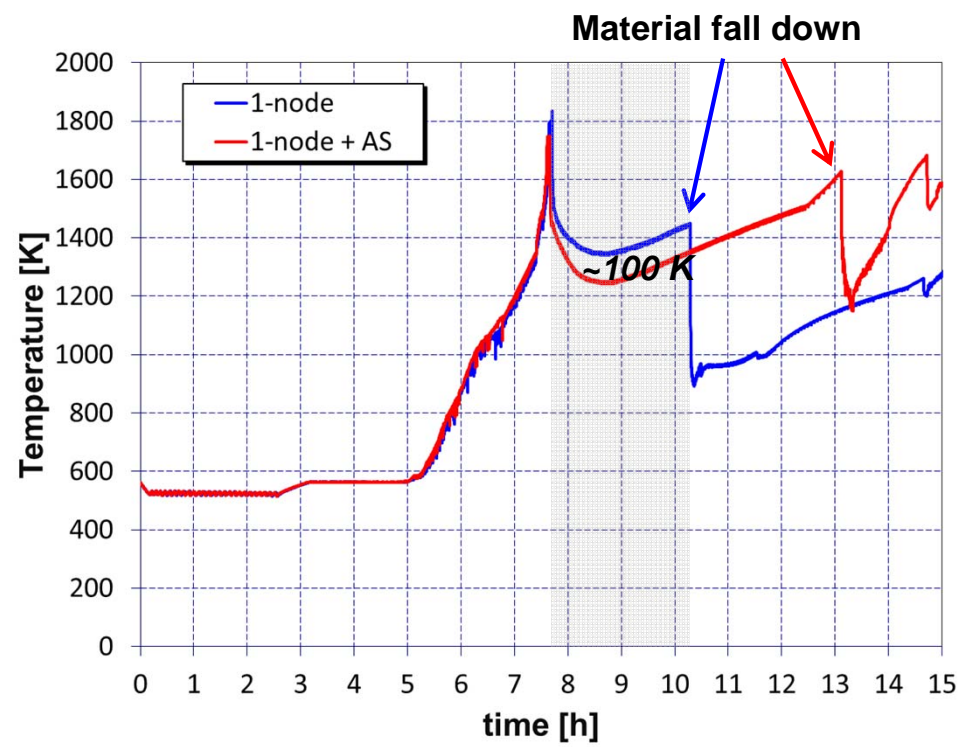


- A second flow loop is developed in the upper plenum
- This loop is broken when SRVs open
- Occasionally this loop can change the direction

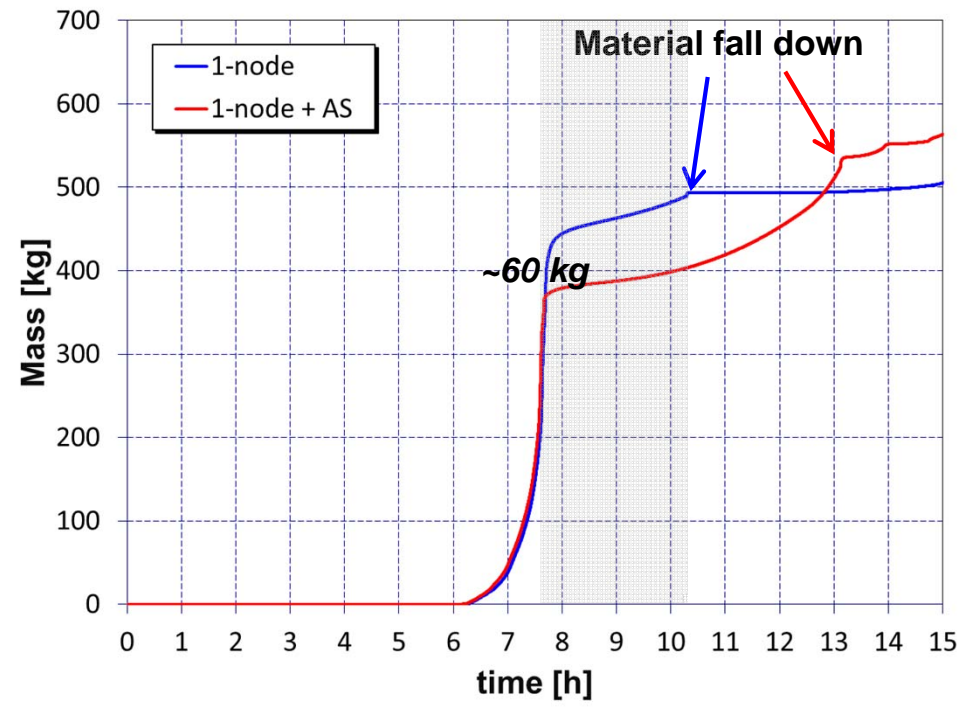


IV. In-vessel insights

Channel temperature

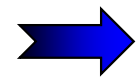


Hydrogen generation



Lower flows leads to higher temperature

Higher temper. leads to higher oxidation

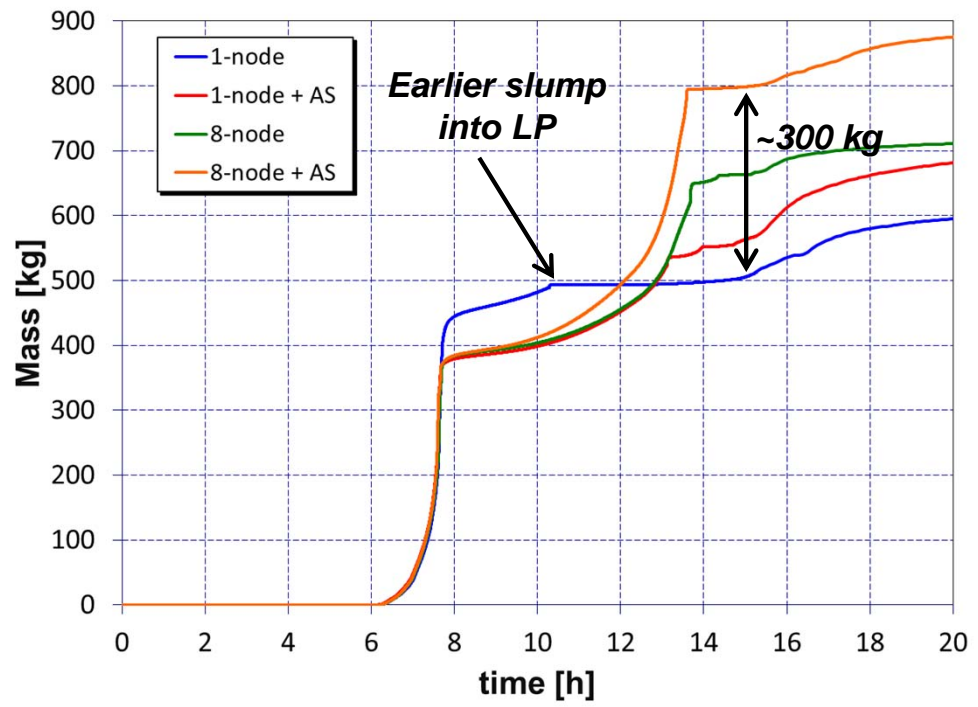


Advanced degradation

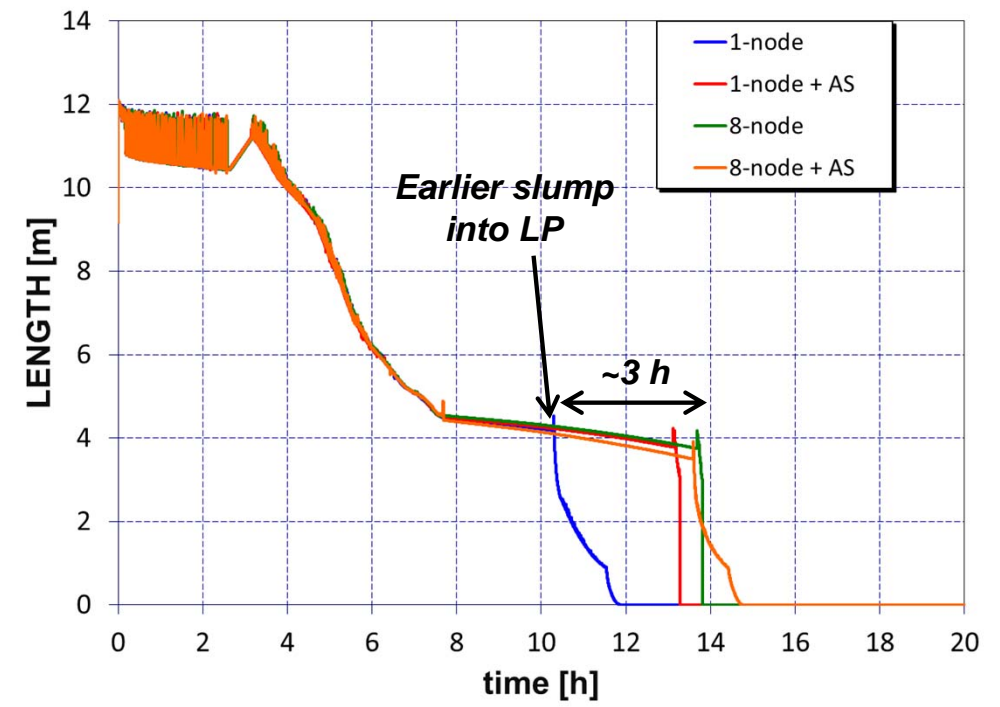


IV. In-vessel insights

H₂ production



Water level



Advanced degradation, leads to lower in-vessel oxidation and earlier RPV dry-out





V. Final remarks

- RPV modeling introduces significant user effect on core degradation evolution.
- Canister failure leads to the development of convective loops inside the RPV.
- Small differences in estimated degradation can lead to significant differences in key parameters, e.g. generated H₂, PCV failure time, etc.
- Results must be taken with caution when supporting accident management.





Acknowledgements

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