# MELCOR Validation against Experiments on Hydrogen Deflagration



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> 3<sup>rd</sup> European MELCOR User Group Meeting Bologna, Italy, April 11-12, 2011

### Outline

- ISP-49 MELCOR Application
- Testing of BUR Package
  - Flame propagation
  - Baby case
  - Problems in modeling of deflagration
- Results of THAI HD-2R simulations
- Summary and Conclusions



### ISP-49 MELCOR Application NRI Participation



- Main objectives
  - Validation of code against experiments
  - User experience extension to H2 deflagration topic

#### ISP-49 - two kinds of experiments

- THAI Facility slow deflagration
  - Operated by Becker Technology (Germany)
  - Main interest of NRI (participation in OECD THAI Project)
- ENACCEF Facility flame front acceleration
  - Operated by CNRS (France)
  - Minor interest, because MELCOR has no models for Flame Acceleration



#### ISP-49 MELCOR Application Slow Hydrogen Deflagration

#### OECD ISP-49 THAI Tests

- No internals (only measurement)
- Deflagration ignited in bottom
- Homogenized atmosphere
- HD-2R Test open calculation
  - H2 concentration 8.0%vol. without steam; temp. 25° C; press. 1.5 bar
- HD-22 Test blind and post-blind calc.
  - H2 concentration 10.0%vol. with 25%vol. steam; temp. 90° C; press. 1.5 bar





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#### NRI MELCOR Model Hydrogen Deflagration Tests

- New input model developed for MELCOR code for OECD-THAI HD test simulation
  - 13 Axial levels, 7 CVs in layer (79+4 CVs, 204 FLs, and 143 HSs)
- Identification of important error in burn propagation among CVs
  - OECD THAI data cannot be shared outside of project members ⇒ Baby Case input model developed for demonstration of error to SNL developers







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#### Flame Propagation Standard MELCOR 1.8.6 YT

End of burn in bottom CV

#### Next time step

#### Stars indicate instant burns Identification of important error in burn propagation among CVs OECD THAI data cannot be shared outside of project members ⇒ Baby Case input model developed for demonstration of \* \* \* \* error to SNL \* developers \* \* H2 Mole Fraction [-] -9.00E-02 \* \* \* -6.00E-02 ⋟ -2.00E-02 -0.00E+00 J. Duspiva 3rd EMUG 6

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#### Baby Case Nodalization Schemes

- Baby case
  - Pipeline with ID 100 mm length 10,200 mm and wall thickness 15 mm
  - First part (200 mm) as space with igniter
- Burning pipe with igniter space
  - End of deflagration should be similar in both models
- 2 CVs model
  - Deflagration propagates from CV020 to CV050
- 6 CVs model
  - Deflagration has to propagate consequently from CV020 to CV051, CV052 ...









#### Baby Case Results Standard MELCOR 1.8.6 YT

- 2 CVs model
  - Deflagration initiated at t<sub>0</sub> = 0.0 s
  - Propagation from CV020 to CV050 at t<sub>1</sub> = 0.0155 s
  - End of deflagration in CV050 at t<sub>2</sub> = 1.573 s
- 6 CVs model
  - Deflagration initiated at t<sub>0</sub> = 0.0 s
  - But at time t<sub>1</sub> = 0.0155 s deflagration propagated into all remaining CVs simultaneously <u>representation algorithm</u>
  - End of deflagration in all CV05i at  $t_2 = 0.326 s$



#### Baby Case Results Improvement of MELCOR 1.8.6

- NRI debugging of this error resulted in identification of correction needs in two routines (<u>burprp.f</u> and <u>burrun.f</u>)
  - Deflagration initiated at  $t_0 = 0.0 s$

#### Standard M186

 Propagation into CV051 1.59547E-02 s

 Propagation into CV052 1.59547E-02 s

 Propagation into CV053 1.59547E-02 s

 Propagation into CV054 1.59547E-02 s

 Propagation into CV055 1.59547E-02 s

 End in CV055 3.36495E-01 s

#### End time in 2CVs model t<sub>2</sub> = 1.573 s Improved M186

Propagation into	CV051	1.59547E-02	s
Propagation into	CV052	3.41714E-01	s
Propagation into	CV053	7.11714E-01	s
Propagation into	CV054	1.06171E+00	s
Propagation into	CV055	1.40171E+00	s
End in CV055		1.73171E+00	S

- Observations and modifications reported to SNL developers including Baby Case inputs (BUG Report 287)
  - Added refilling of burning tube with hydrogen and oxygen and initiation of subsequent deflagration => second set of deflagrations again propagated into all CVs simultaneously, one more routine modified (burcom.f) to correct subsequent deflagrations

CV020	CV051	CV052	CV053	CV054	CV055
\$ <mark></mark> *	R \$51	R. \$52	FL 0 53	R.054	FL 0 55
111111111	///////////////////////////////////////		///////////////////////////////////////		///////////////////////////////////////
HS02001	HS05101	HS05201	HS05301	HS05401	HS05501



#### Flame Propagation Standard MELCOR

- NRI performed set of other tests
  - Testing of older version (MELCOR1.8.5) against baby case with additional source of hydrogen (SNL modification)
    - MELGEN failed due to incompleteness of hydrogen source definition
    - MELGEN YT\_1010 and YU\_2798 do not check existence of appropriate external energy source related to external mass source as described on page CVH-UG-26 (full description in BUG339 report from end of February 2009)
    - MELCOR 1.8.6 (and also 2.1) corrected to fulfill request on existence of external energy source for each of external mass source
    - It is solved in subversion 3037 of M186 and 1191 of M2.1
  - Additional testing of propagation with standard H2 Mole Fraction [-] release of MELCOR 1.8.6 YT\_1010
    - Zero hydrogen concentration in one (or more) of CVs on propagation chain of CVs preserve remaining CVs from immediate deflagration propagation
      - Important for older Cntn analyses



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#### Modeling of Deflagration Problematic Topics

- Some problematic topics identified in MELCOR application to THAI HD-2R test
  - Significantly faster flame propagation
    - Flame speed determination
  - Remaining unburnt hydrogen
    - Effect of lumped parameter approach to combustion completeness
  - Rate of hydrogen consumed from burning



#### Modeling of Deflagration Flame Speed Determination

- MELCOR uses only one correlation for all flame directions (upward, downward, and horizontal)
- NRI prepared updated definition of SC2200 for application within ISP-49
  - Based on OECD THAI HD tests
    - Proprietary source
  - Relevant only for upward flame propagation
    - It cannot be recommended for plant simulations
  - It played important role in HD-22 test simulation, where underpredicted flame velocity resulted in absence of deflagration in central nodes of upper half of vessel
    - Corrected with realistic flame velocity 
       impact of ATM overflow



#### Modeling of Deflagration Lumped Parameter Approach

- Full combustion completeness is defined ⇒ H2 mole fraction is 0.0 at the end of deflagration in lower CV
- Continuation of deflagration in adjacent CV results in ATM pressurization in recently burning CV and its expansion
   Image: Source of the second s
- MELCOR code does not distinguish atmosphere composition in front and behind flame front position -ATM is fully homogeneous
- Due to instant combustion, ATM flowing into other CVs is
  - H2 lean in comparison with CV in front of flame front propagation (here above) ⇒ decrease of H2 mole fraction
  - H2 rich in comparison with CV behind flame front (here below) increase of H2 content, which remains unburnt





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### Modeling of Deflagration Lumped Parameter Approach

- Full combustion completeness is defined ⇒ H2 mole fraction is 0.0 at the end of deflagration in lower CV
- Continuation of deflagration in adjacent CV results in ATM pressurization in recently burning CV and its expansion
   overflow into all adjacent CVs
- MELCOR code does not distinguish atmosphere composition in front and behind flame front position -ATM is fully homogeneous
- Due to instant combustion, ATM flowing into other CVs is
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### Modeling of Deflagration Lumped Parameter Approach

- Is it possible to find any user solution?
  - MELCOR has no capability to filter one or more ATM components in flow paths ⇒ No
    - More over MELCOR does not know orientation of flame movement and position of sides – in front and behind flame front (volumetric combustion approach)

  - MELCOR has capability to define igniter in each of cell ⇒ Possible user solution (necessary modification of some model parameters - XH2IGY, XH2CC, and XH2PDN)
- Is complicated nodalization best approach for MELCOR?
  - More variants of nodalization prepared and tested
  - Some models had also subversions
  - Results processing focused on timing of flame front position, pressure evolution, and unburnt mass of hydrogen





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#### Modeling of Deflagration Hydrogen Removal Rate

Pressure

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- Duration of deflagration is calculated from characteristic dimension (of control volume) and flame speed
- Flame speed is calculated from concentrations at beginning of burn, but
- Rate of hydrogen consumed from burning is calculated from current concentrations in each time step and it is proceeded in whole volume
  - Real burn is proportional to surface of flame front (spherical shape)
- Deflagration is terminated after predicted duration (point 1)

H2 Removal Mass Rate

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 Those effects occurred in all CVs and in all input models, but in this case is very well visible



#### Simulation of HD-2R Test Impact of Nodalization

- 5 nodalizations prepared
- Specific user approaches defined
  - S&S H2 sinks defined behind flame front and appropriate sources in front of it
  - Ign igniters in CV behind flame front



#### Simulation of HD-2R Test Impact of Nodalization

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Best agreement between simulation and measured pressure history

- Maximum pressure 5CVs
- The simplest case 4CVs (usual approach to Cntn) slightly overestimated pressure maximum and significantly earlier onset of pressure increase - immediate deflagration in big volume
- Cases with additional igniters 5CVs+Ign and 79+5CVs+Ign slightly overestimated pressure maximum, but they predict correctly combustion completness

 Probably due to underestimation of heat losses from flame front to walls (absence of radiation)



### Summary and Conclusions

#### • Validation of MELCOR code against deflagration tests resulted in

- Code correction flame propagation algorithm
- Observations concerning problems with more detail nodalizations
  - LP approach effect redistribution of H2 to already burnt CVs
  - Flame speed prediction using default correlation
  - Rate of hydrogen removal during deflagration
  - Code has no modeling capability for flame acceleration
- It is not possible to suppose any improvement without important and principal changes of source code and BUR package model, but
- Code is flexible
  - It allows to define more realistic flame speed profile via. CF (if it is known)
  - It allows to use some user approaches (if user knows results)



## Summary and Conclusions

- Generally H2 deflagration is important, but deflagration itself is very fast process and its very detail modeling within whole plant simulation seems not be necessary
  - But LP effect could influence prediction of H2 distribution in detail Cntn nodalizations, if any deflagration is predicted
- Integral application of MELCOR code to source term estimation in scenario with hydrogen deflagration is possible
  - Duration of deflagration is very short in comparison with whole scenario
  - Whole plant input models include usually coarse nodalization (more rooms are merged into one CV or one CV per room) - case 4CVs showed relatively good agreement in maximum pressure
- H2 distribution requests very detailed nodalization, but it results in absolutely wrong prediction of deflagration
  - Study on impact of nodalization is needed
  - MELCOR is not suitable code for detailed study of H2 combustion



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# Conclusions on Cntn Modelling

- User has to anticipate convection loops in containment, mainly in large open space (reactor hall) and to develop nodalization with taking of such loops into account
  - Only one CV for reactor hall can't simulate any circulation
- Recommendation on FL definition between virtually subdivided big space
  - Prepared by Dr. Sonnenkalb (GRS) based on comparison of MELCOR to COCOSYS
    - Presentation at the  $1^{st}$  EMUG Meeting 12/2008
    - FLARA reduced to max 20 m2, FLLEN max 10 m
    - In my THAI model I used real values of FLARA, FLLEN, SAREA, and SLEN, but in Cntn I used reduced values for SLEN (0.1 m)





## **Conclusions on Cntn Modelling**

- OECD THAI Project Benchmark on HM2 test
  - Recommendation to model CVs and FLs of upward directed plumes
    - Flow is directed with pressure difference, which depends on hydrostatic head and it is function of atmosphere density
    - If light gas enters to big volume, it is immediately homogenized with content of this CV, but
    - If upward plume is simulated with independent set of CVs, pressure difference is kept and buoyant force is predicted correctly
    - Problematic topic angle depends on plume and ATM composition, but
      - They vary during plant simulations, but nodalization is fixed



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