



DETAILS OF THE ACCIDENT PROGRESSION IN 1F1 EMUG 2019

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Switzerland, 3rd -5th April 2019

MELCOR 1.8.6 Model for 1F1

- **Not part of the BSAF OECD Benchmark Project**
 - ◆ Relying exclusively on publically available input data
 - ◆ No legal restraints for usage & publication (**project and export control**)

- **Aim is to reproduce 1F1 accident with low (minimum) number of fit parameters**
 - ◆ Prefer physical models over forced boundary conditions
 - ◆ No 1:1 correspondence to measured data desired

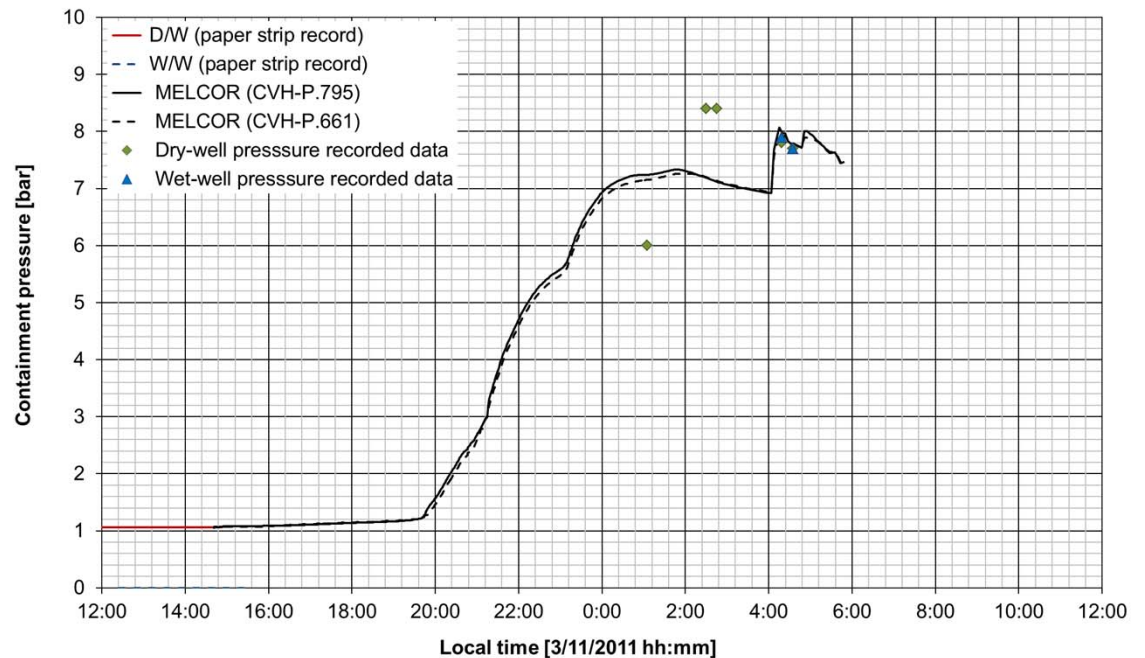
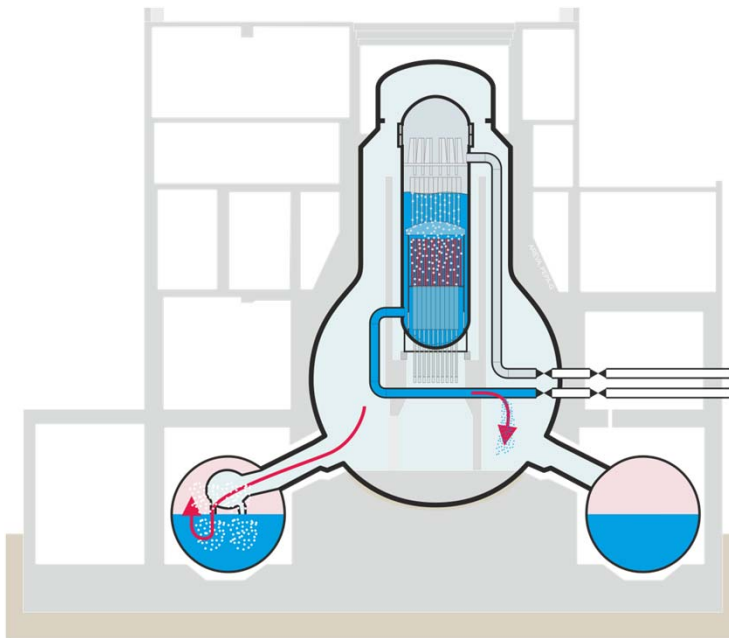
- **TEST MODEL – not a HOW-TO – Handle with care**
 - ◆ Alternative untested / not recommended modelling techniques
 - ◆ Test base for conversion 1.8.6 to 2.x

- **Model & description report freely distributed to MELCOR community (FGF_D02-ARV-01-111-828)**
 - ◆ **Revision B** (hardcopy) on EMUG2018
 - ◆ **Revision C** the MELCOR input model at CSARP/MCAP 2018
 - ◆ **Revision D planned end 2019**

RCS Leakage before RPV Failure? (I of II)

- Containment pressure 6 bar-abs at 12th March 01:00

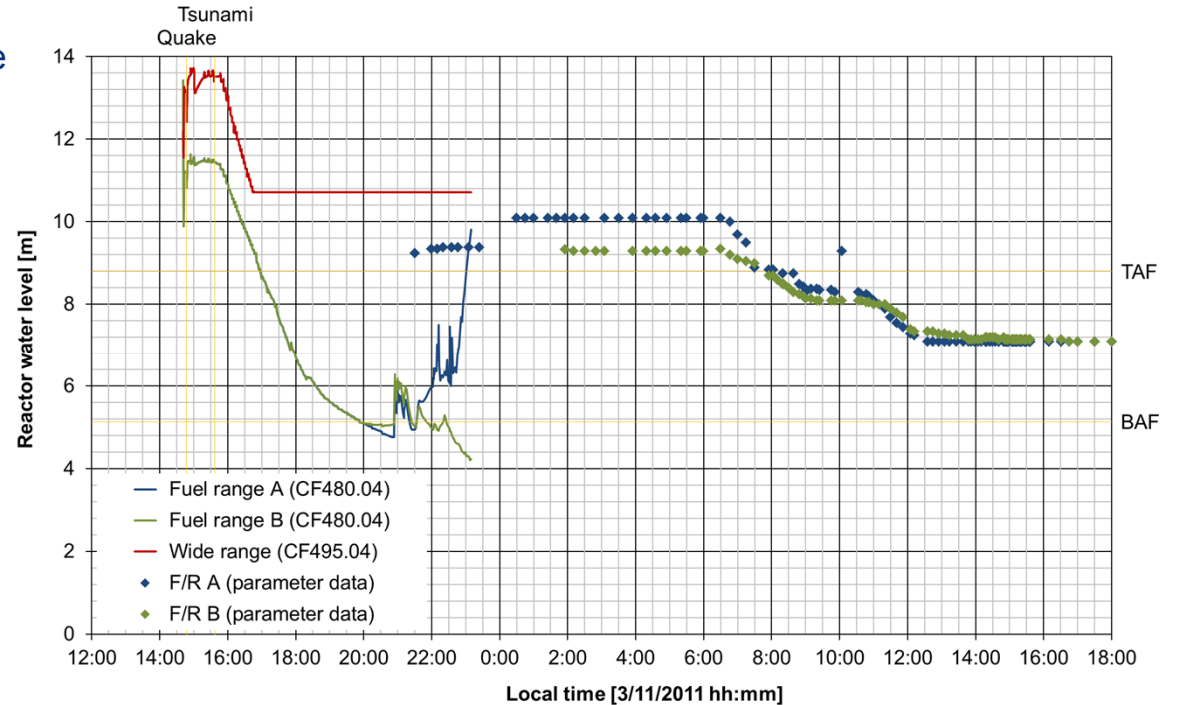
- ◆ Likely that RPV failure occurs afterward
- ◆ A discharge only via open SRV into the W/W would require > 1500 kg H₂ (100% core oxidation) to fill W/W and D/W
- ◆ A steam leak in the D/W compresses N₂ + H₂ into the W/W requiring ~ 500-800 kg H₂



RCS Leakage before RPV Failure? (II of II)

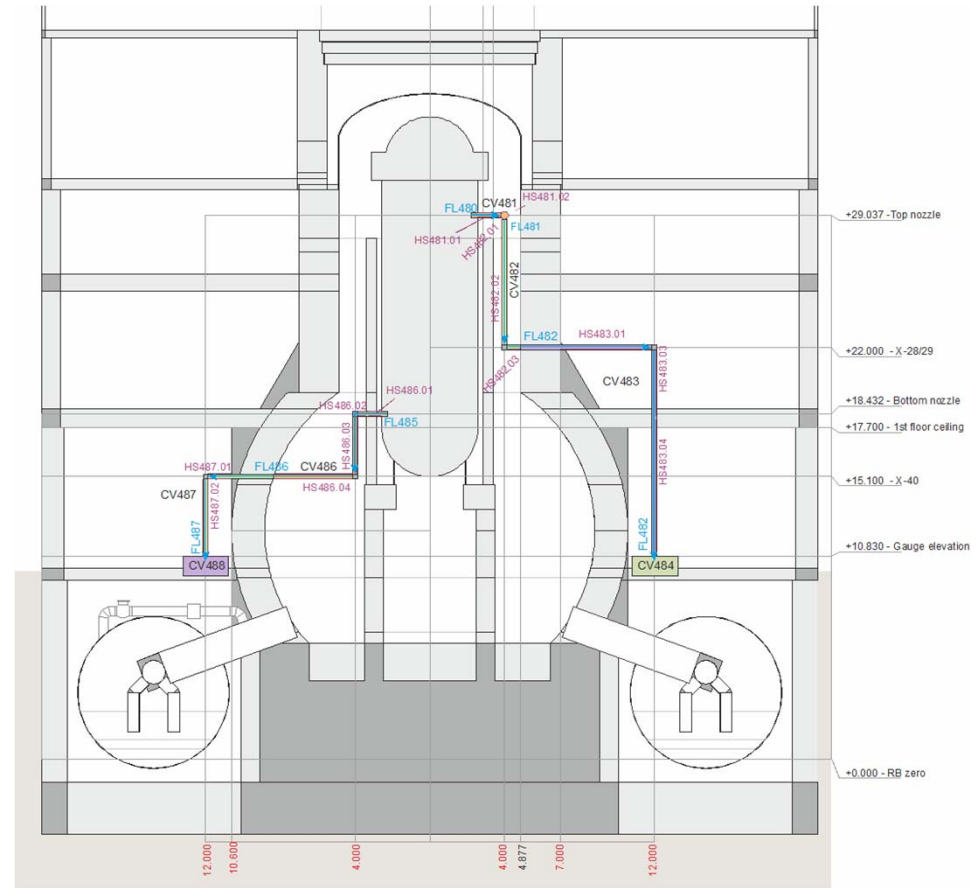
■ Malfunctioning of RPV water level measurement

- ◆ Containment heat-up via insulated RCS unlikely to be sufficient to cause this malfunctioning
- ◆ **RCS leakage before 11th March 21:30**
- ◆ Dry-out of upper reference line, and very late dry-out of lower sensing line
- ▶ Leak can not be too large



Test Leakage Scenarios via Response of the RPV Level Measurement

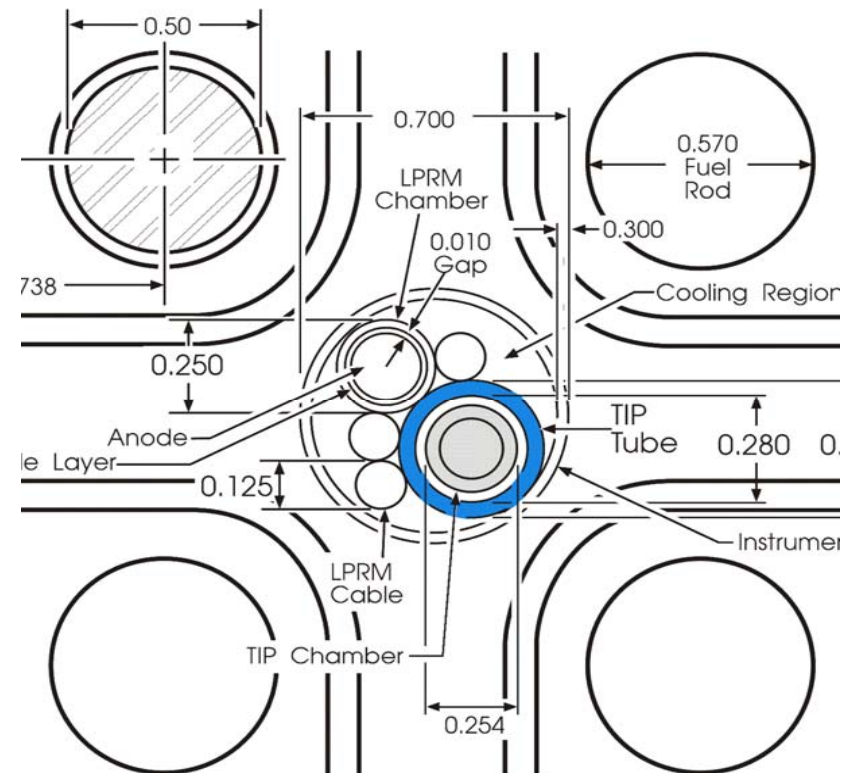
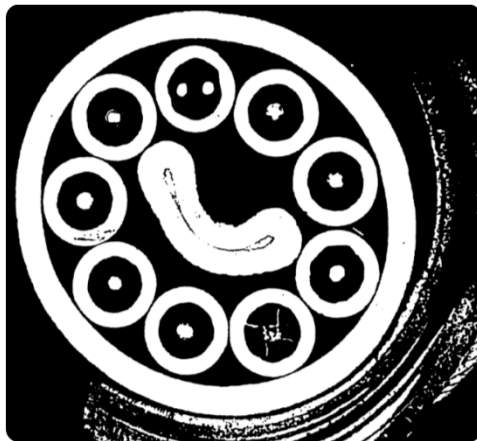
- **Modelling of RPV water level measurement**
 - ◆ Generic 0.5 inch schedule 80 piping
 - ◆ No detailed information about piping routing available
 - ◆ Limited accuracy !!!!
- **Complementary to TEPCO 5th Progress Report Attachment 1-6 Gothic simulation of containment**
 - https://www7.tepco.co.jp/newsroom/press/archives/2017/1485273_10469.html
 - https://www4.tepco.co.jp/en/press/corp-com/release/betu17_e/images/171225e0213.pdf



Failure of In-core Dry Tubes (I of II)

■ TIP dry tube failure?

- ◆ Dry tubes open to containment, reach from below into core regions
- ◆ Free cross section of 22 lances ~9 cm²
- ◆ Highly likely that these dry-tubes get damaged by core overheating
- ◆ Uncertain what real leakage cross section is



Three Mile Island Accident of Knowledge Database NUREG/KM-0001,
<https://www.nrc.gov/reading-rm/doc-collections/nuregs/knowledge/km0001/r1/>

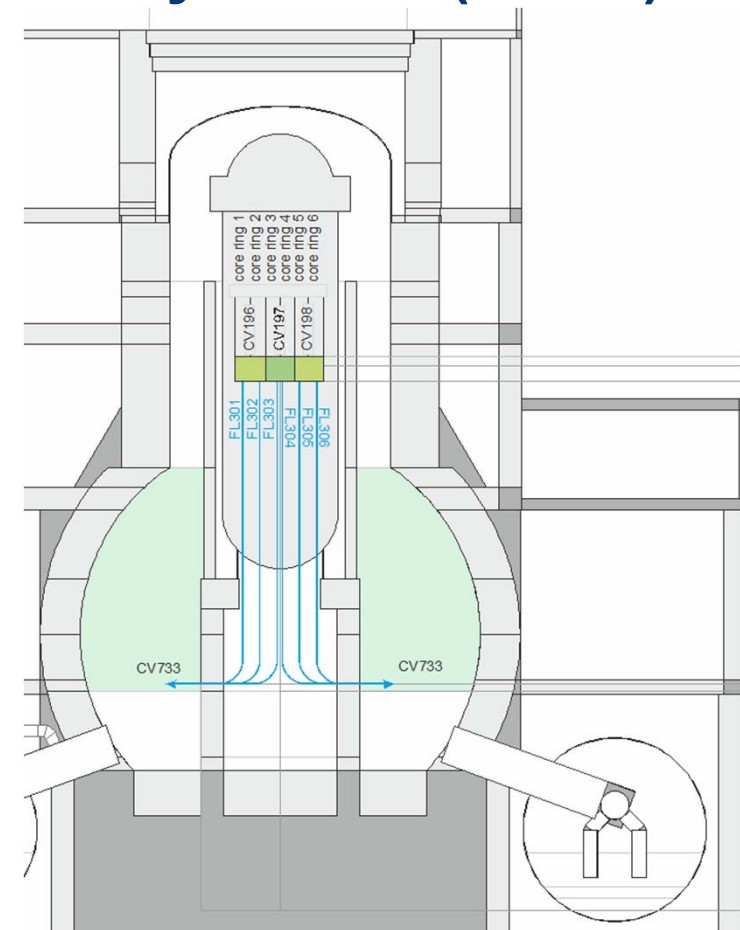
Failure of In-core Dry Tubes (II of II)

■ TIP dry tube failure?

- ◆ Dry tubes fail in ring when bypass fluid temperature $> 1400^{\circ}\text{C}$
- ◆ Steam leakage
- ◆ Leakage of failed tubes: 10% of free area (bounding high assumption)
- ◆ Pipe length ~ 20 m, squeezed over first 20 cm, DHYD = 0.001



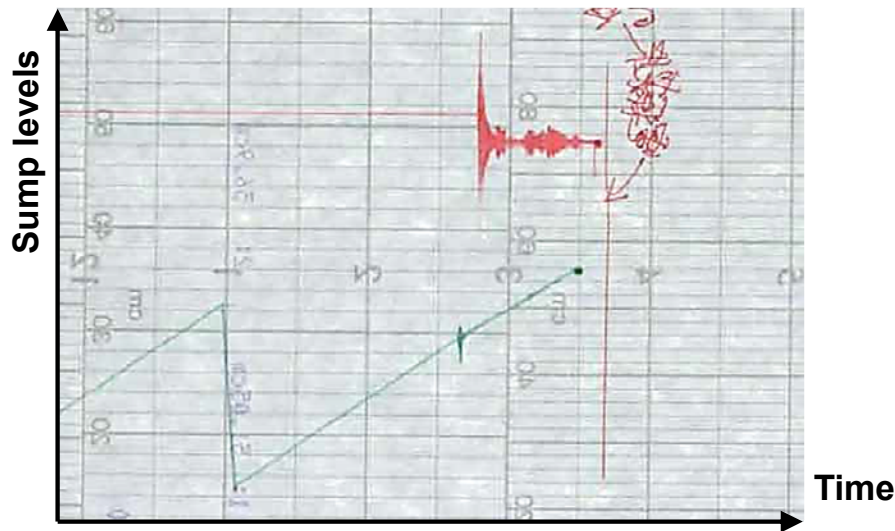
-► **Highly likely that leakage occurs, but flow is expected to be too small to cause level measurement malfunctioning**



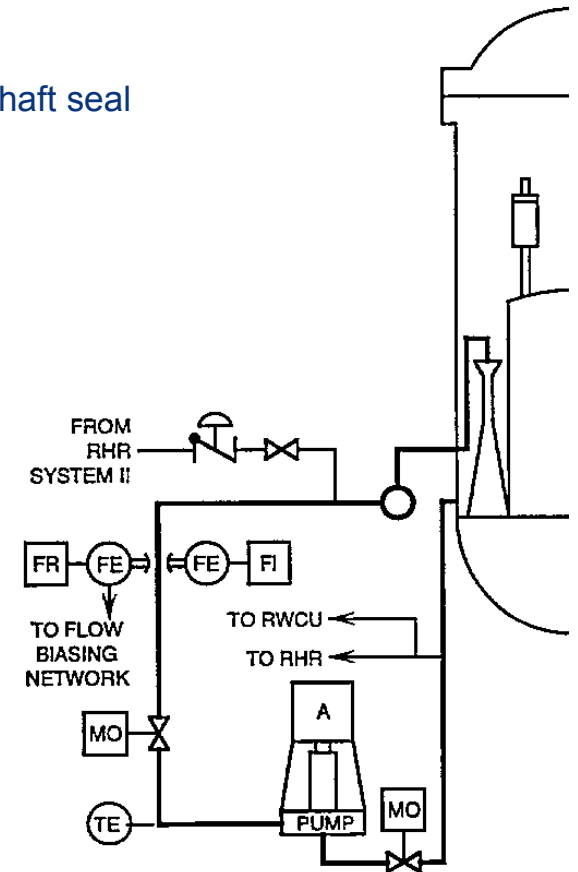
Recirculation Pump Seal Leakage (I of II)

Recirculation pumps seal failure?

- ◆ Control rod drive hydraulic system injects ~3 gpm cold water per pump into shaft seal
- ◆ Most enter RCS, some leaks to the outside
- ◆ Leakage low / high alarm < 0.25 / > 0.9 gpm per pump
- ◆ 1F1 equipment sump level rise -> 0.71 gpm => 0.04 kg/s per pump



Plant Data published by TEPCO <https://www4.tepco.co.jp/en/nu/fukushima-np/index10-e.html>



Recirculation Pump Seal Leakage (II of II)

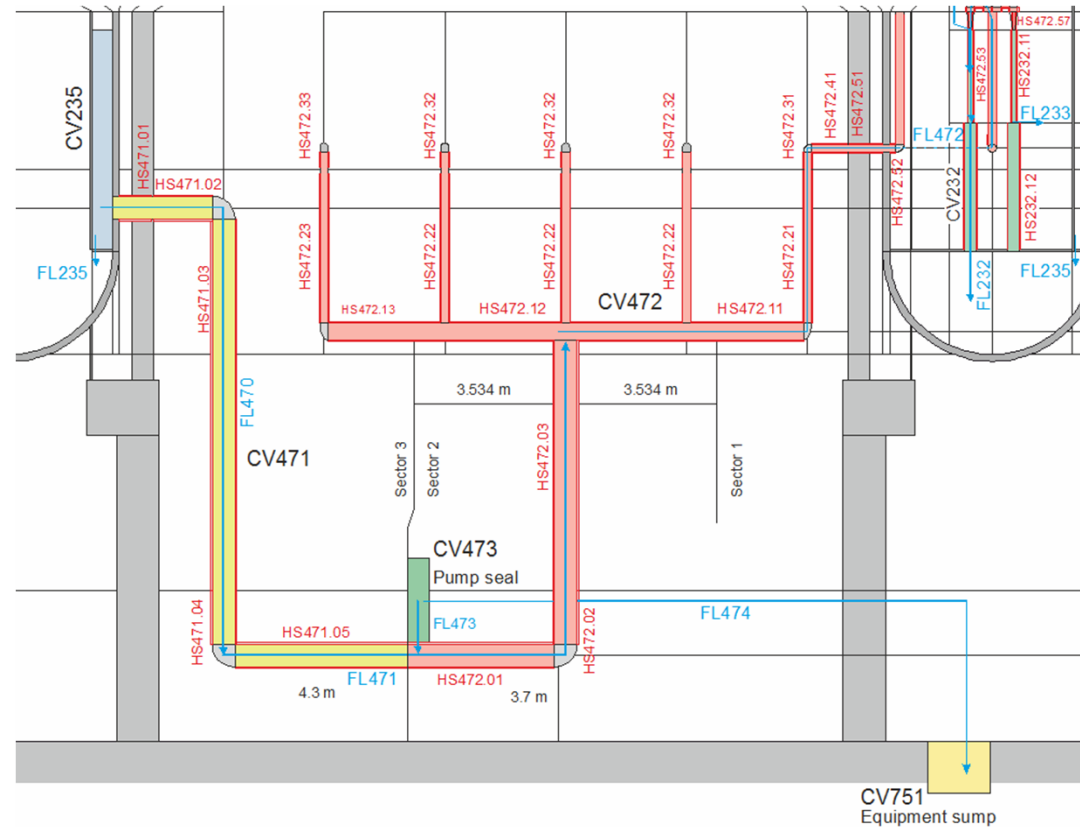
■ In SBO condition

- ◆ Pump seals designed for 160°F ~71°C
- ◆ With loss of AC power pump seal cooling stops, possibility causing thermal damage of seals
- ◆ In SBO / overheating tests, no significant leakages were observed (NUREG/CR-4821)
- ◆ Theoretical max. leakage 100 gpm / 6 kg/s
- ◆ Observed operational BWR seal leakages (NUREG-1401) mostly < 10 gpm / 0.6 kg/s

■ Steam leakage would be saturated

- ◆ Can not cause a dry-out of the RPV liquid level measurement

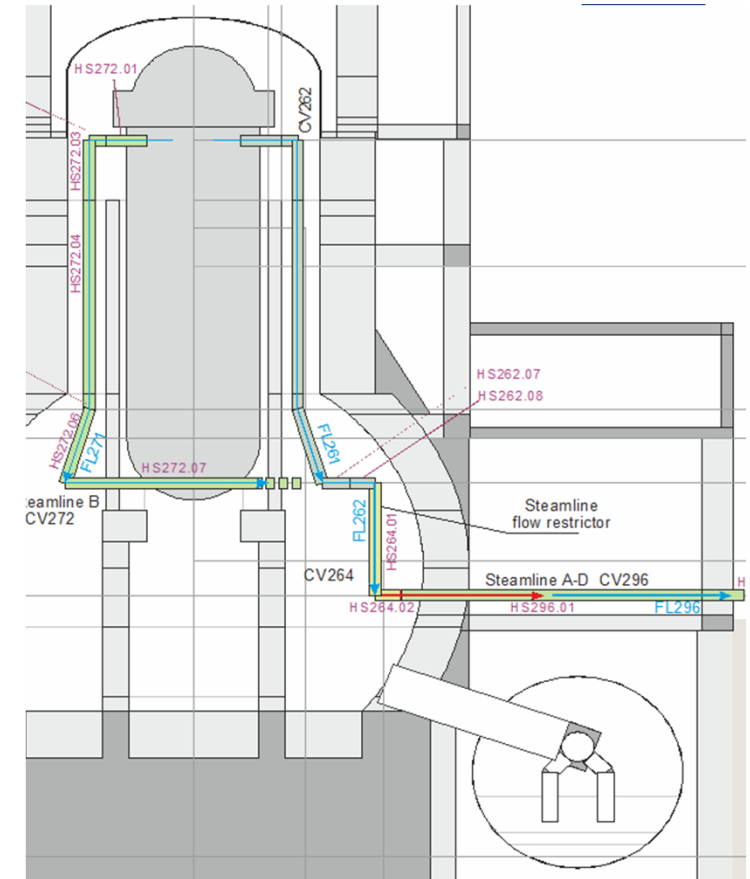
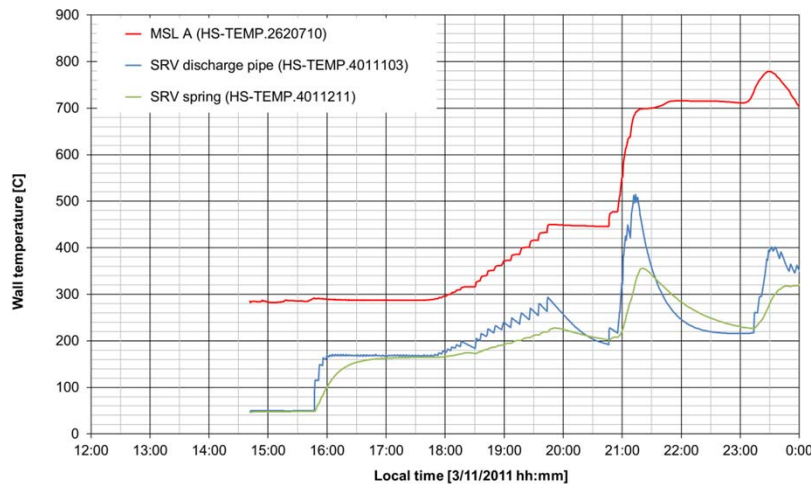
-► Increase of pump seal leakage in 1F1 appears currently unlikely, but not finally resolved, but it cant cause dry-out of level measurement lines



Creep Rupture of Main Steam Pipe (I of II)

■ Main steam lines

- ◆ Transports steam from RPV to turbine
- ◆ 18 inch schedule 80 piping, thermally insulated
- ◆ Closed off by main steam isolation valves
- ◆ Reach ~700°C up to 21:30 on the March 11th
- ◆ No continuous flow from RPV
 - ▶ superheated core gas can cool in steam separator & dryer

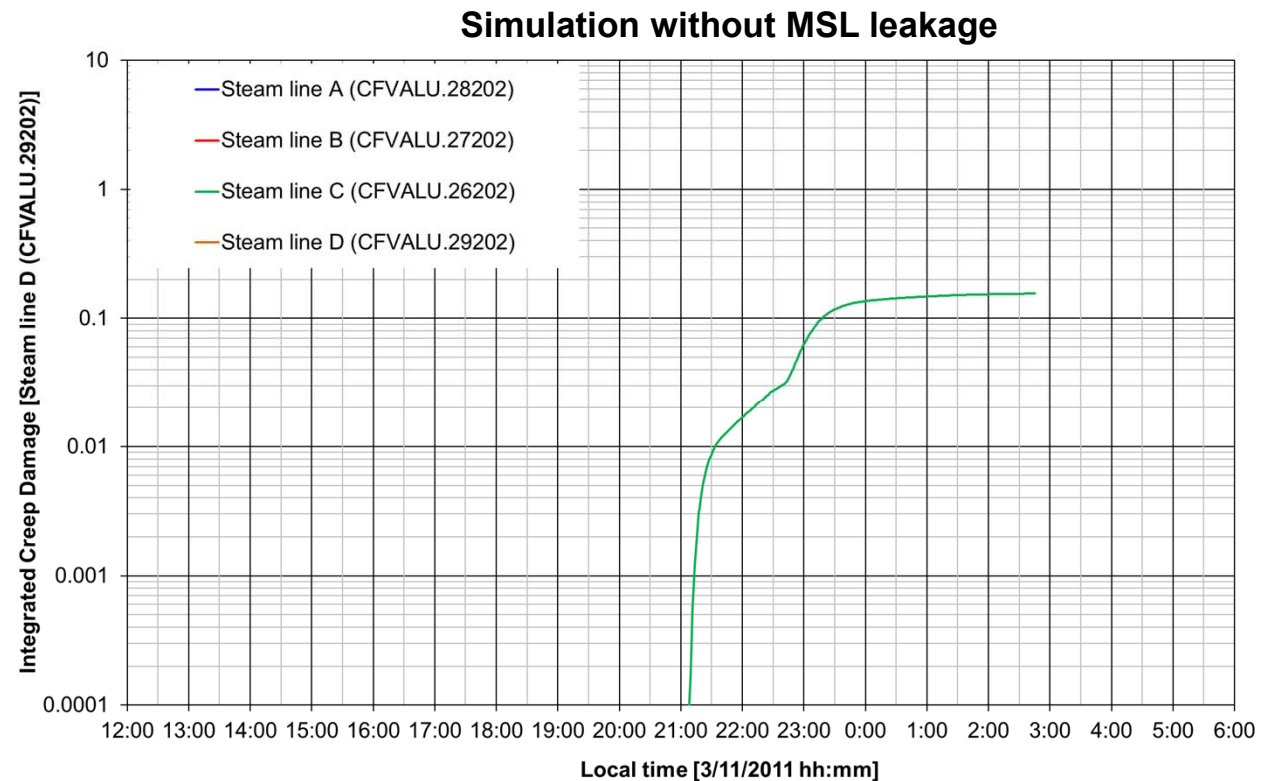


Creep Rupture of Main Steam Pipe (II of II)

- At ~ 700°C only limited creep damage

- ◆ ~1% creep damage up to 21:30
- ◆ unlikely that pipe failed that early

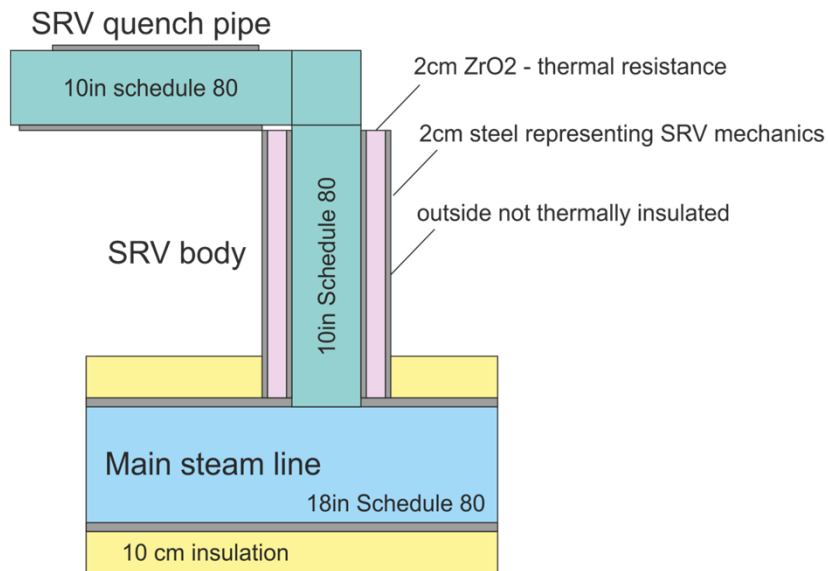
-> If main steam pipe failed early on, then likely not by rupturing but at measurement penetrations (compare LHF4, OLHF4) resulting in small leakage



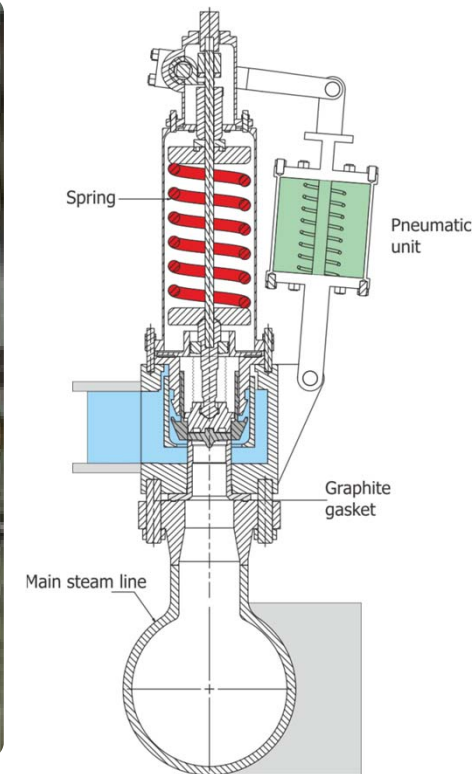
Failure of Safety Relief Valves (I of V)

■ Safety relief valves

- ◆ Relief function by pneumatic cylinder
- ◆ Safety function by spring
- ◆ Flanged with graphite gasket (design temperature 450°C)
- ◆ Dump steam into suppression pool via 10 inch pipes



TEPCO Photo & Video Library
<https://www7.tepco.co.jp/library/index-e.html>



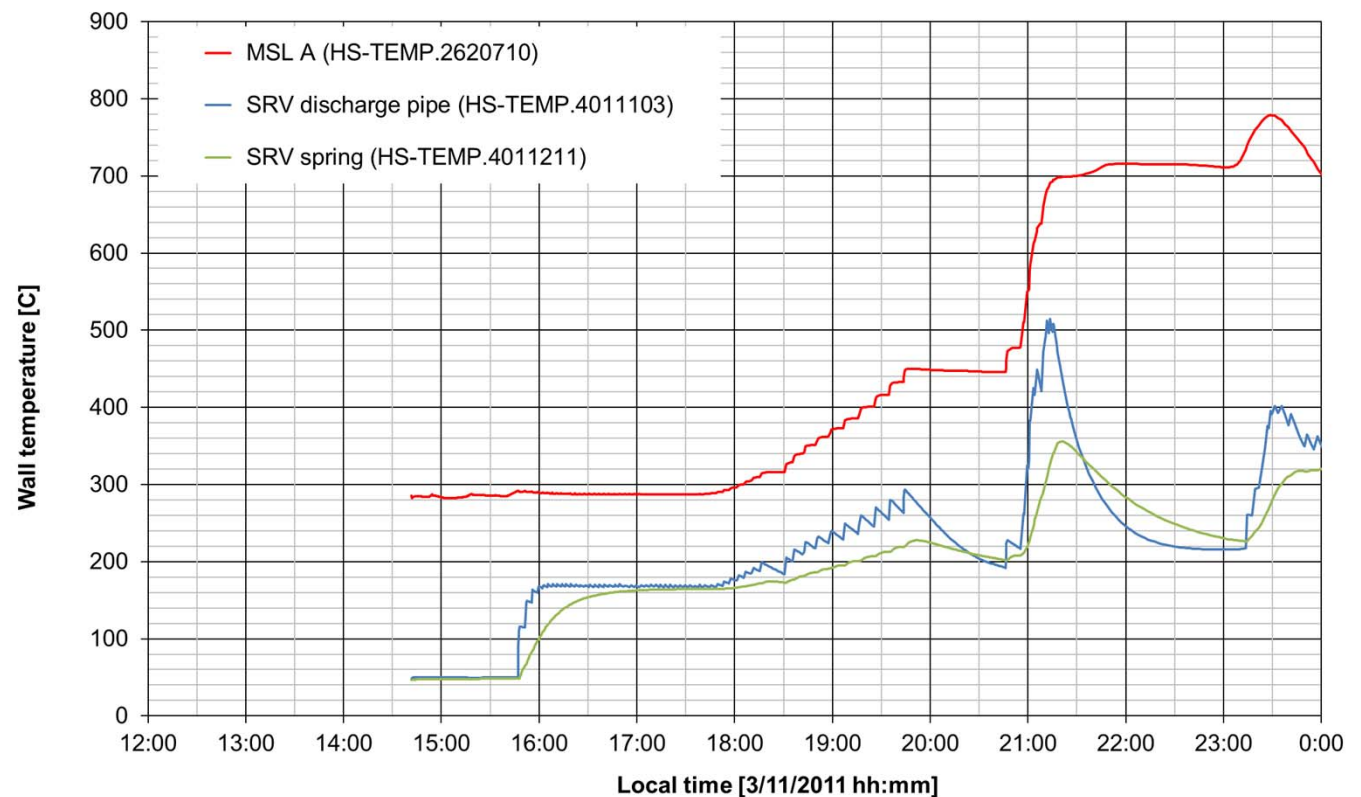
Failure of Safety Relief Valves (II of V)

■ Simulation temperatures

- ◆ SRV body shortly above 500°C
- ◆ SRV mechanics cooler ~200°C up to 20:00

■ Why so “low” temperatures

- ◆ Non-insulated
 - heat loss to PCV
- ◆ No continuous flow from RPV
 - superheated core gas can cool in steam separator & dryer



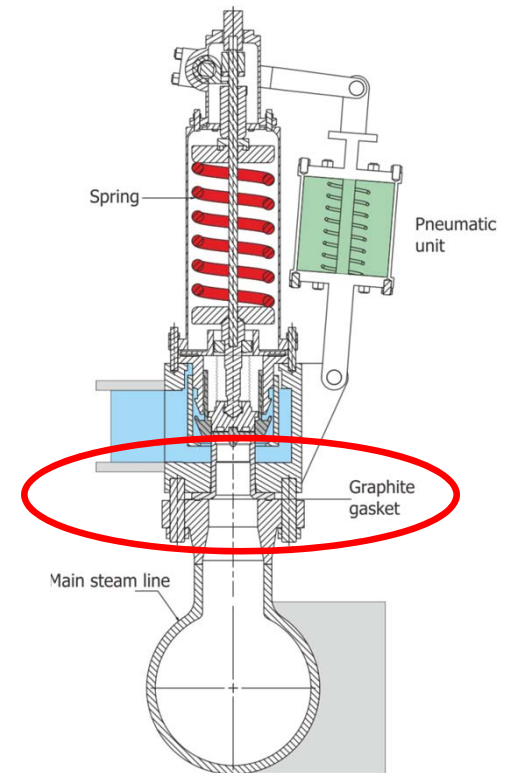
Failure of Safety Relief Valves (III of V)

■ SRV gasket failure?

- ◆ In simulation, SRV temperature (450°C) exceeded for < 15 min
- ◆ **Exceeding the design does not mean failure**
- ◆ > 700°C graphite gets oxidized (slowly) by steam

-► **Highly unlikely that SRV gasket started leaking**

GRAFOIL® Flexible Graphite Engineering Design Manual
In gasketing conditions, the 975°F (525°C) temperature should not be considered a maximum use temperature in air but merely a “caution flag” that requires further examination of the operation. The thin-edge exposure of GRAFOIL packings and gaskets has successfully withstood extended periods of exposure to air at process fluid temperatures up to 1500°F (815°C).

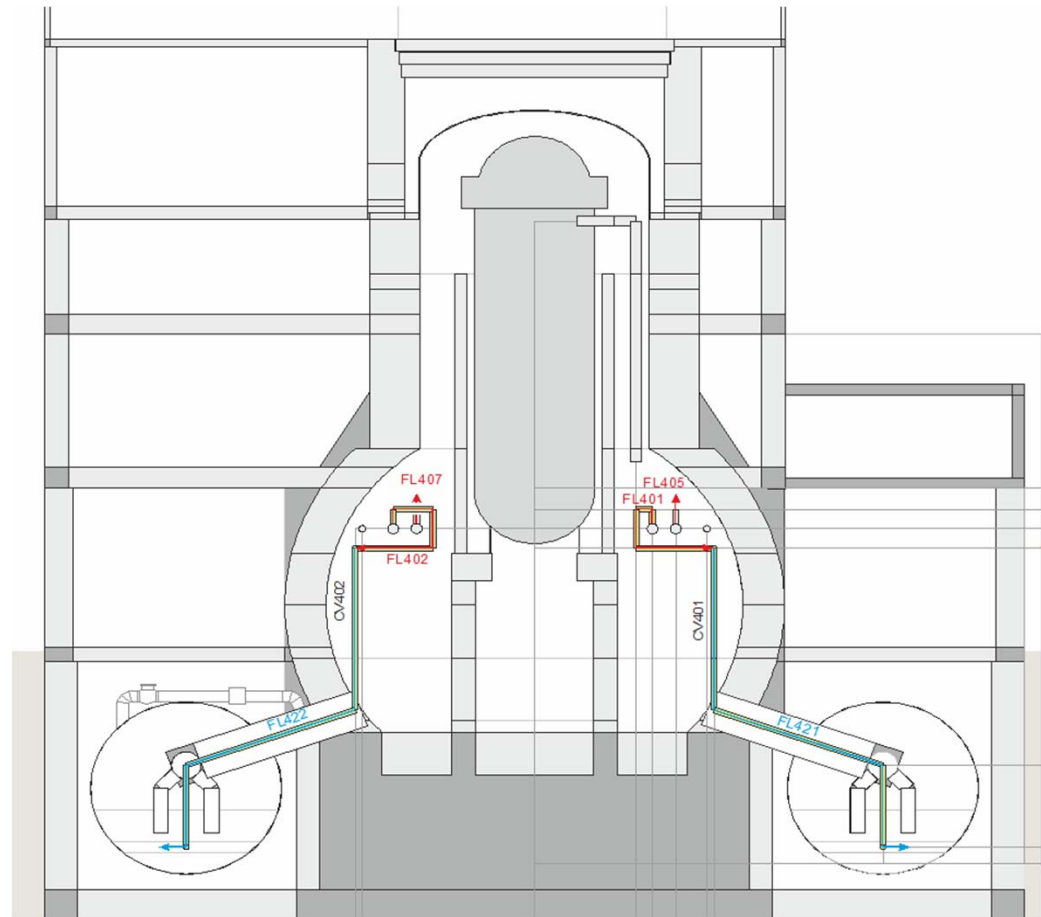


Failure of Safety Relief Valves (IV of V)

■ SRV stuck-open?

- ◆ In simulation, SRV body $> 450^{\circ}\text{C}$ for < 15 min
- ◆ Design exceeding, but probably able to stand heat load
- ◆ Stuck-open failure would not lead to a heat-up of the PCV atmosphere
- ◆ Inconsistent to high containment pressure

-> **Appears unlikely that SRV failed in open position**

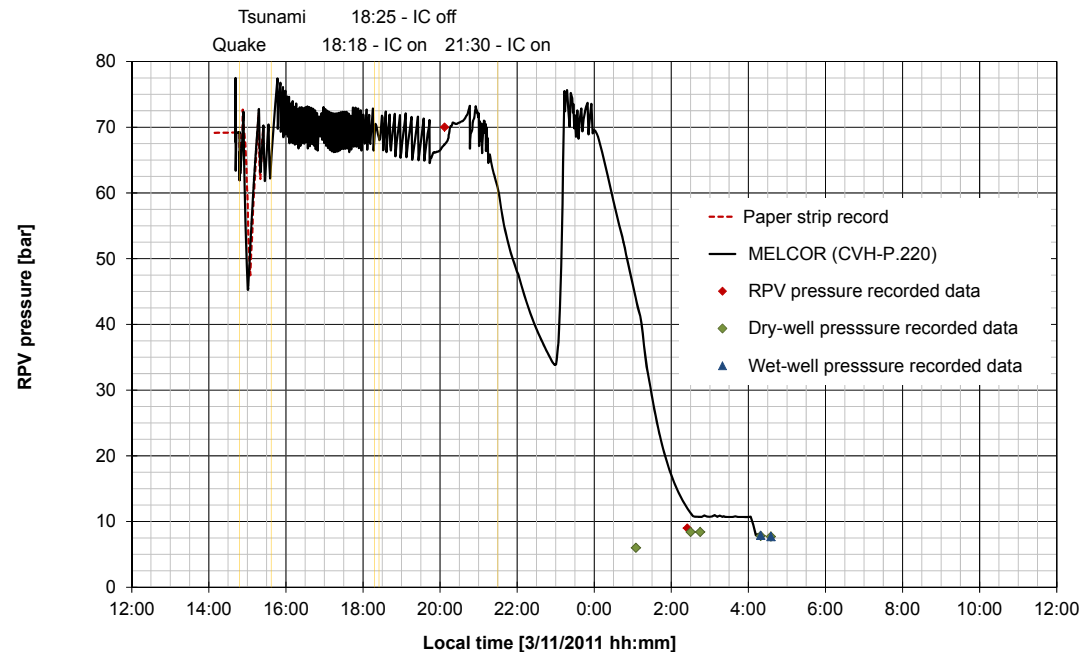


Failure of Safety Relief Valves (V of V)

■ Shift of actuation pressure?

- ◆ Relief function open **72.7** barg / close **69.7** barg relative to environment
- ◆ Safety function open **76.4** barg / close **68.8** barg relative to containment (PCV) atmosphere
- ◆ Pressure measurement at 20:07 **69** barg
- ◆ Measured pressure just at the lower edge of the SRV safety opening band (possible but unlikely)
- ◆ When pressure is kept via safety valves, PCV pressure causes rise in RPV pressure
- ◆ Safety function defined by steel spring
- ◆ Heat-up reduces steel Young's module ~ 4%/100K
- ◆ RPV spring temperature 150°C -> 250°C
-> SRV set-points ~73 barg and 66 barg

-▶ **Likely that heat-up of SRV body caused slight decrease in actuation pressure**



Summary (I of II)

■ Indications for RCS failure long before RPV failure

- ◆ Malfunctioning of the RPV liquid level measurement at March 11th 21:30
- ◆ Containment pressure buildup to 6 bar-abs at 12th March 01:00, thus before RPV failure was likely

■ Damage to the TIP dry tubes

- ◆ Highly likely that damage occurred as these pipes reach within the core
- ◆ Unknown cross section after squeezing flat
- ◆ TIP failure alone cannot explain the faulty level measurement

■ Failure of the pump seals

- ◆ Currently appears unlikely, but inconclusive
- ◆ Releases steam < 180°C, can contribute to pressure buildup, but not to dry-out of RPV level sensing lines

■ Failure of the SRV graphite gaskets

- ◆ Occurrence is highly unlikely due to temperature resistance of gaskets

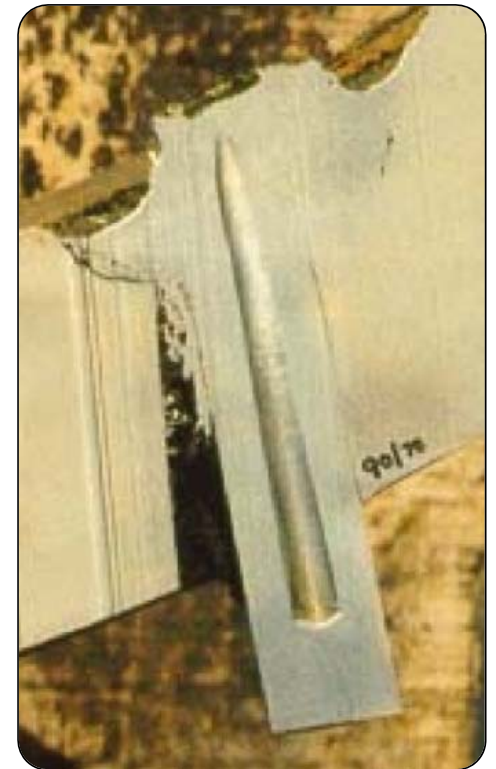
Summary (II of II)

- **Failure of SRV in open position**
 - ◆ More unlikely as no extremely high temperature loads
 - ◆ No indications of this occurrence in the containment response
 - ◆ A fail-open would not lead to the observed liquid level measurement failure

- **Large Rupture of main steam line due to creep**
 - ◆ Appears unlikely, especially in the early stages
 - ◆ Can not explain the liquid level measurement failure at 21:30

- **Most Likely: Instrumentation penetration failure of the main steam line**
 - ◆ Small leakage of few cm² sufficient to cause level measurement failure when failure location in the upper containment
 - ◆ Consistent scenario with the TEPCO Gothic analysis

- **Additionally: Shift of the SRV pressure set-points due to heat-up**
 - ◆ Can explain the 69 bar RPV pressure measurement at 20:07
 - ◆ Will not lead to a substantial depressurization of the RCS, not to level malfunctioning and not to containment pressure rise



OECD Lower Head Failure Project
<https://www.oecd-nea.org/nsd/docs/2002/csni-r2002-27.pdf>

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